



January 31, 2019



William F. Durham, Director WVDEP Division of Air Quality 601 57th Street SE Charleston, WV 25304

RE: R13 Permit Application

Curtisville #50 Compressor Station

Facility ID No: 049-00052

Dear Mr. Durham:

Equitrans, LP (Equitrans) is submitting this R13 modification application for its natural gas compressor station located in Marion County, West Virginia ("Curtisville Compressor Station). This station is currently operating under permits R30-049-00052-2013 and G60-C084. This permit application is being filed to replace a dehydration unit at the compressor station.

With this enclosed application, Equitrans has attached the appropriate forms for the application as well as the \$1000 application fee check made payable to the "WVDEP – Division of Air Quality."

Equitrans appreciates your review of this application. If you have any questions or comments about the attached information or have additional information requirements, please feel free to contact me at (412) 400-6887 or at KrRyan@equitransmidstream.com.

Sincerely,

Kristin Ryan

Manager, Environmental



PROJECT REPORT

Equitrans, LP > Curtisville Compressor Station

€ equitrans Midstream

Marion County, West Virginia

Prepared By:

TRINITY CONSULTANTS
4500 Brooktree Rd.
Suite 103
Wexford, PA 15090
(724) 935-2611

January 2019



Environmental solutions delivered uncommonly well

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Equitrans, LP (Equitrans) is submitting this modification application to the West Virginia Department of Environmental Protection (WVDEP) for the natural gas compressor station located in Marion County, West Virginia (Curtisville Compressor Station). Specifically, this application seeks authorization to install a new dehydration unit and associated enclosed combustor to replace the existing dehydration unit. The Curtisville Compressor Station is currently operating in accordance with WVDEP Title V Operating Permit No. R30-04900052-2017, issued on October 30, 2017.

1.1. FACILITY AND PROJECT DESCRIPTION

The Curtisville Compressor Station is a natural gas transmission facility covered under Standard Industrial Classification (SIC) code 4922. The facility has the potential to operate 24 hours per day, and 7 days per week. The station is currently permitted for the following equipment:

- > One (1) natural gas fired Clark HRA8 compressor engine, rated at 1,100 horsepower (hp);
- > One (1) natural gas fired Kohler 50-RZ generator engine, rated at 125 hp;
- > One (1) natural gas fired Kohler 25REZG emergency generator engine, rated at 44 hp;
- One (1) natural gas fired heating boiler, rated at 1.25 MMBtu/hr;
- One (1) triethylene glycol (TEG) dehydration unit rated at 35 million standard cubic feet per day (MMSCFD) with associated reboiler (rated at 0.35 MMBtu/hr) and flare (rated at 0.08 MMBtu/hr); and
- Four (4) miscellaneous storage tanks (4,000 gallons or less, each).

With this application, Equitrans is proposing to install a new 60 MMSCFD TEG dehydration unit and associated reboiler (rated at 1.54 MMBtu/hr) to replace the existing unit and reboiler. The new unit will be controlled by an enclosed combustor, rated at 6 MMBtu/hr.

1.2. R-13 APPLICATION ORGANIZATION

This R-13 permit application is organized as follows:

> Section 2: Sample Emission Source Calculations:

Section 3: R-13 Application Form;
 Attachment A: Business Certificate;

> Attachment B: Map;

Attachment C: Installation and Start Up Schedule;

Attachment D: Regulatory Discussion;

Attachment E: Plot Plan:

Attachment F: Detailed Process Flow Diagram;

Attachment G: Process Description;
 Attachment I: Emission Units Table;

Attachment J: Emission Points Data Summary Sheet
 Attachment K: Fugitive Emissions Data Summary Sheet;

> Attachment L: Emissions Unit Data Sheets

Attachment M: Air Pollution Control Device Sheet;
 Attachment N: Supporting Emission Calculations;

Attachment 0: Monitoring/Recordkeeping/Reporting/Testing Plans;

> Attachment P: Public Notice; and

> Attachment S: Title V Permit Revision Information; and

> Application Fee

2. SAMPLE EMISSION SOURCE CALCULATIONS

The proposed changes are limited to volatile organic compound (VOC) and hazardous air pollutant (HAP) emissions from the operation of the dehydration unit. As the proposed project will include the removal of the existing dehydration unit, the overall fugitive component count from the facility is not anticipated to increase as a result of the proposed project.

Potential emissions of HAPs, VOC, and methane from the proposed dehydration unit are calculated using GRI-GLYCalc. Emissions of other criteria pollutants are calculated for natural gas combustion in the enclosed combustor and reboiler using U.S. EPA's AP-42 factors for external combustion of natural gas. Greenhouse gas emissions from combustion in the combustor and reboiler are calculated according to the procedures in 40 CFR 98 Subpart C.

The WVDEP permit application forms contained in this application include all applicable R13 application forms including the required attachments.

WFST VIRGINIA DEPARTMENT OF **ENVIRONMENTAL PROTECTION DIVISION OF AIR QUALITY**

APPLICATION FOR NSR PERMIT AND

601 57th Street, SE Charleston, WV 25304 (304) 926-0475 www.dep.wv.gov/daq	Т	TITLE V PERMIT REVISION (OPTIONAL)					
PLEASE CHECK ALL THAT APPLY TO NSR (45CSR13) (IF KN	OWN): PLEASE CHEC	CK TYPE OF 45CSR30 (TITLE V) REVISION (IF ANY					
☑ CONSTRUCTION ☐ MODIFICATION ☐ RELOCATION	1 -	RATIVE AMENDMENT					
CLASS I ADMINISTRATIVE UPDATE TEMPORARY	- IE ANN DOV AD	NT MODIFICATION					
CLASS II ADMINISTRATIVE UPDATE AFTER-THE-FA		BOVE IS CHECKED, INCLUDE TITLE V REVISION N AS ATTACHMENT S TO THIS APPLICATION					
FOR TITLE V FACILITIES ONLY: Please refer to "Title V (Appendix A, "Title V Permit Revision Flowchart") and a	Revision Guidance" in o ability to operate with the	order to determine your Title V Revision options he changes requested in this Permit Application.					
Sec	tion I. General						
Name of applicant (as registered with the WV Secretar Equitrans, LP	y of State's Office):	Federal Employer ID No. (FEIN): 25-0724685					
3. Name of facility (if different from above):		4. The applicant is the:					
Curtisville #50 Compressor Station		☐ OWNER ☐ OPERATOR ☑ BOTH					
5A. Applicant's mailing address: 2200 Energy Dr. Canonsburg, PA 15317		esent physical address: oad, Mannington District N					
 6. West Virginia Business Registration. Is the applicant If YES, provide a copy of the Certificate of Incorpora change amendments or other Business Registration C If NO, provide a copy of the Certificate of Authority/A amendments or other Business Certificate as Attachn 	ntion/Organization/Lim Certificate as Attachme Authority of L.L.C./Re	mited Partnership (one page) including any nament A.					
7. If applicant is a subsidiary corporation, please provide tl	he name of parent corp	poration: EQT Corporation					
8. Does the applicant own, lease, have an option to buy or	r otherwise have contro	rol of the proposed site? XYES NO					
If YES, please explain: Applicant owns site If NO you are not elimible for a possit footbig source.							
 If NO, you are not eligible for a permit for this source. 							
 Type of plant or facility (stationary source) to be const administratively updated or temporarily permitted or crusher, etc.): Natural Gas Compressor Station 							
11A. DAQ Plant ID No. (for existing facilities only): 049-00052		CSR13 and 45CSR30 (Title V) permit numbers his process (for existing facilities only):					
All of the required forms and additional information can be for	ound under the Permittin	ing Section of DAQ's website, or requested by phon					

12A.		
For Modifications, Administrative Updates or Te present location of the facility from the nearest state	mporary permits at an existing facility, e road;	please provide directions to the
For Construction or Relocation permits, please proad. Include a MAP as Attachment B.	rovide directions to the proposed new s	site location from the nearest state
From Mannington, take Buffalo St (Rte 1) heading to follow for about 1 mile. Turn right on Laurel Run Ro	west for approximately 5 miles. Turn lef I. Entrans to station is 1000 feet on the	t on Curtisville Pike (Rte 7) and right.
12.B. New site address (if applicable):	12C. Nearest city or town:	12D. County:
Laurel Run Road	Mannington	Marion
12.E. UTM Northing (KM): 4,375.025	12F. UTM Easting (KM): 548.149	12G. UTM Zone: 17
 Briefly describe the proposed change(s) at the facility Equitrans is proposing to replace the existing dehydration enclosed combustor. 	n unit and flare with a new 60 MMscfd u	nit, associated reboiler, and
14A. Provide the date of anticipated installation or change		14B. Date of anticipated Start-Up
If this is an After-The-Fact permit application, provi change did happen: / /	de the date upon which the proposed	if a permit is granted: ASAP
14C. Provide a Schedule of the planned Installation of/0 application as Attachment C (if more than one unit		units proposed in this permit
15. Provide maximum projected Operating Schedule of Hours Per Day 24 Days Per Week 7	activity/activities outlined in this application Weeks Per Year 52	ation:
16. Is demolition or physical renovation at an existing fac-	cility involved?	
17. Risk Management Plans. If this facility is subject to	112(r) of the 1990 CAAA, or will becom	e subject due to proposed
changes (for applicability help see www.epa.gov/cepp	o), submit your Risk Management Pla i	n (RMP) to U. S. EPA Region III.
18. Regulatory Discussion. List all Federal and State a	ir pollution control regulations that you b	pelieve are applicable to the
proposed process (if known). A list of possible applica	ble requirements is also included in Atta	achment S of this application
(Title V Permit Revision Information). Discuss applicat	oility and proposed demonstration(s) of	compliance (if known). Provide this
information as Attachment D.		
Section II. Additional atta	chments and supporting do	ocuments.
 Include a check payable to WVDEP – Division of Air (45CSR13). 	Quality with the appropriate application	fee (per 45CSR22 and
20. Include a Table of Contents as the first page of your	r application package.	
21. Provide a Plot Plan , e.g. scaled map(s) and/or sketc source(s) is or is to be located as Attachment E (Re	h(es) showing the location of the proper fer to <i>Plot Plan Guidance</i>).	rty on which the stationary
 Indicate the location of the nearest occupied structure 	(e.g. church, school, business, residence	ce).
 Provide a Detailed Process Flow Diagram(s) show device as Attachment F. 	ng each proposed or modified emission	s unit, emission point and control
23. Provide a Process Description as Attachment G.		
 Also describe and quantify to the extent possible a 		V
All of the required forms and additional information can be	found under the Permitting Section of DA	Q's website, or requested by phone.
 24. Provide Material Safety Data Sheets (MSDS) for all For chemical processes, provide a MSDS for each cor 		as Attachment H.
25. Fill out the Emission Units Table and provide it as A	-	
26. Fill out the Emission Points Data Summary Sheet		Attachment J.

27.	Fill out the Fugitive Emissions Data S	Summary Sheet and provide it	as Attachment K.
28.	Check all applicable Emissions Unit E	Data Sheets listed below	
	Bulk Liquid Transfer Operations	☐ Haul Road Emissions	☐ Quarry
	Chemical Processes	☐ Hot Mix Asphalt Plant	☐ Solid Materials Sizing, Handling and Storage
	Concrete Batch Plant	☐ Incinerator	Facilities
	Grey Iron and Steel Foundry	☐ Indirect Heat Exchanger	Storage Tanks
⊠ (General Emission Unit, specify : TEG De	ehydration Unit	
Fill	out and provide the Emissions Unit Da	ta Sheet(s) as Attachment L.	
29.	Check all applicable Air Pollution Cor	trol Device Sheets listed below	N:
	Absorption Systems	☐ Baghouse	⊠ Flare
	Adsorption Systems	☐ Condenser	☐ Mechanical Collector
	Afterburner	☐ Electrostatic Precipitat	or Wet Collecting System
	Other Collectors, specify		
Fill	out and provide the Air Pollution Cont	rol Device Sheet(s) as Attachr	nent M.
30.	Provide all Supporting Emissions Ca Items 28 through 31.	Iculations as Attachment N, o	r attach the calculations directly to the forms listed in
31.		ompliance with the proposed er	proposed monitoring, recordkeeping, reporting and nissions limits and operating parameters in this permit
>		not be able to accept all measu	ner or not the applicant chooses to propose such res proposed by the applicant. If none of these plans the definition of the permit.
32.	Public Notice. At the time that the ap	plication is submitted, place a C	lass i Legal Advertisement in a newspaper of general
	circulation in the area where the source	e is or will be located (See 45Cs	SR§13-8.3 through 45CSR§13-8.5 and Example Legal
	Advertisement for details). Please su	bmit the Affidavit of Publication	n as Attachment P immediately upon receipt.
33.	Business Confidentiality Claims. Do	es this application include conf	dential information (per 45CSR31)?
	☐ YES	⊠ NO	
>		the criteria under 45CSR§31-4	nitted as confidential and provide justification for each 1.1, and in accordance with the DAQ's "Precautionary instructions as Attachment Q.
	Sec	tion III. Certification o	f Information
34.	Authority/Delegation of Authority. Check applicable Authority Form belo		ner than the responsible official signs the application.
	Authority of Corporation or Other Busine	ess Entity	Authority of Partnership
	Authority of Governmental Agency		Authority of Limited Partnership
	omit completed and signed Authority Fo		
			ermitting Section of DAQ's website, or requested by phone.

35A. Certification of Information. To certify 2.28) or Authorized Representative shall chec	this permit application, a Responsible Offick the appropriate box and sign below.	cial (per 45CSR§13-2.22 and 45CSR§30-								
Certification of Truth, Accuracy, and Comp	pleteness									
I, the undersigned Responsible Official / application and any supporting documents appreasonable inquiry I further agree to assume restationary source described herein in accorda Environmental Protection, Division of Air Qual and regulations of the West Virginia Division of business or agency changes its Responsible on the official of the official	pended hereto, is true, accurate, and compresponsibility for the construction, modifications with this application and any amendmelity permit issued in accordance with this application and any amendment of Air Quality and W.Va. Code § 22-5-1 et sofficial or Authorized Representative, the Design of the Expresentative.	plete based on information and belief after tion and/or relocation and operation of the ents thereto, as well as the Department of oplication, along with all applicable rules see. (State Air Pollution Control Act). If the								
Compliance Certification										
Except for requirements identified in the Title \text{\text{that, based on information and belief formed a compliance with all applicable requirements.} SIGNATURE	after reasonable inquiry, all air contaminant	chieved, I, the undersigned hereby certify sources identified in this application are in DATE: (Please use blue ink)								
(Please	use blue ink)	(Please use blue ink)								
35B. Printed name of signee: Jack Mackin		35C. Title: Vice President of Operations								
35D. E-mail: JaMackin@equitransmidstream.com	36E. Phone:	36F. FAX:								
36A. Printed name of contact person (if different	ent from above): Nevin Edwards	36B. Title: Engineer II								
36C. E-mail: NeEdwards@equitransmidstream.com	36D. Phone: 724-271-7793	36E. FAX:								
PLEASE CHECK ALL APPLICABLE ATTACHMEN	ITS INCLUDED WITH THIS PERMIT APPLICAT	TON:								
PLEASE CHECK ALL APPLICABLE ATTACHMENTS INCLUDED WITH THIS PERMIT APPLICATION: Attachment A: Business Certificate Attachment B: Map(s) Attachment C: Installation and Start Up Schedule Attachment C: Installation and Start Up Schedule Attachment D: Regulatory Discussion Attachment D: Regulatory Discussion Attachment B: Plot Plan Attachment C: Detailed Process Flow Diagram(s) Attachment F: Detailed Process Flow Diagram(s) Attachment G: Process Description Attachment B: Material Safety Data Sheets (MSDS) Attachment C: Business Confidential Claims Attachment C: Business Confident										
FOR AGENCY USE ONLY - IF THIS IS A TITLE V	SOURCE									
 □ Forward 1 copy of the application to the Title □ For Title V Administrative Amendments: □ NSR permit writer should notify Title V □ For Title V Minor Modifications: 	N Permitting Group and: V permit writer of draft permit, Topriate notification to EPA and affected state V permit writer of draft permit. Ed in parallel with NSR Permit revision: Ed V permit writer of draft permit,	es within 5 days of receipt,								
☐ EPA has 45 day review period of a draw	ft permit.	n of DAQ's website, or requested by phone								



ATTACHMENT A

Current Business Certificate

WEST VIRGINIA STATE TAX DEPARTMENT BUSINESS REGISTRATION CERTIFICATE

ISSUED TO:
EQUITRANS LIMITED PARTNERSHIP
DBA EQT MIDSTREAM
1710 PENNSYLVANIA AVE
CHARLESTON, WV 25302-3934

BUSINESS REGISTRATION ACCOUNT NUMBER:

1023-5643

This certificate is issued on:

06/22/2011

This certificate is issued by the West Virginia State Tax Commissioner in accordance with Chapter 11, Article 12, of the West Virginia Code

The person or organization identified on this certificate is registered to conduct business in the State of West Virginia at the location above.

This certificate is not transferrable and must be displayed at the location for which issued. This certificate shall be permanent until cessation of the business for which the certificate of registration was granted or until it is suspended, revoked or cancelled by the Tax Commissioner.

Change in name or change of location shall be considered a cessation of the business and a new certificate shall be required.

TRAVELING/STREET VENDORS: Must carry a copy of this certificate in every vehicle operated by them. CONTRACTORS, DRILLING OPERATORS, TIMBER/LOGGING OPERATIONS: Must have a copy of this certificate displayed at every job site within West Virginia.

atL006 v.4 L1891744896

ATTACHMENT B

Map

ATTACHMENT B - AREA MAP



Figure 1 - Map of Curtisville Station

UTM Northing (KM): 4,375.025 UTM Easting (KM): 548.149

ATTACHMENT C

Startup and Installation Schedule

Schedule of Planned Installation and Start-Up

Installation will begin upon issuance	of the permit. Startup	o is anticipated imme	diately once construct	tion is completed.
	\			

ATTACHMENT D

Regulatory Discussion

Regulatory Applicability

This section documents the applicability determinations made for Federal and State air quality regulations. The monitoring, recordkeeping, reporting, and testing plan is presented in Attachment O. In this section, applicability or non-applicability of the following regulatory programs is addressed:

- Prevention of Significant Deterioration (PSD) permitting;
- Title V of the 1990 Clean Air Act Amendments;
- New Source Performance Standards (NSPS);
- National Emission Standards for Hazardous Air Pollutants (NESHAP); and
- West Virginia State Implementation Plan (SIP) regulations.

In addition to providing a summary of applicable requirements, this section of the application also provides non-applicability determinations for certain regulations, allowing the WVDEP to confirm that identified regulations are not applicable to the proposed project. Note that explanations of non-applicability are limited to those regulations for which there may be some question of applicability specific to the operations at the Curtisville Compressor Station. Regulations that are categorically non-applicable are not discussed.

Prevention of Significant Deterioration Source Classification

Federal construction permitting programs regulate new and modified sources of attainment pollutants under PSD and new and modified sources of non-attainment pollutants under Non-Attainment New Source Review (NNSR). PSD and NNSR regulations apply when a major source makes a change, such as installing new equipment or modifying existing equipment, and a significant increase in emissions results from the change. The Curtisville Compressor Station is located in Marion County, which is designated as an attainment area. As such, PSD regulations are applicable.

The Curtisville Compressor Station will remain a minor source with respect to the PSD program after the project since its potential emissions are below all the PSD thresholds. As such, PSD permitting is not triggered by this construction activity.

Title V Operating Permit Program

Title 40 of the Code of Federal Regulations Part 70 (40 CFR 70) establishes the federal Title V operating permit program. West Virginia has incorporated the provisions of this federal program in its Title V operating permit program in West Virginia Code of State Regulations (CSR) 45-30. The major source thresholds with respect to the West Virginia Title V operating permit program regulations are 10 tons per year (tpy) of a single HAP, 25 tpy of any combination of HAP, and 100 tpy of all other regulated pollutants. Potential emissions of NOx exceed 100 tpy. Therefore, the Curtisville Compressor Station is a major source with respect to the Title V permit program. Equitrans has included the necessary Title V application forms in Attachment S to this application to revise the current Title V permit.

New Source Performance Standards

New Source Performance Standards (NSPS), located in 40 CFR 60, require new, modified, or reconstructed sources to control emissions to the level achievable by the best demonstrated technology as specified in the applicable

provisions. Moreover, any source subject to an NSPS is also subject to the general provisions of NSPS Subpart A, except where expressly noted.

Equitrans is proposing to install a new glycol dehydrator as part of this project. The proposed glycol dehydrator is not an affected facility under potentially applicable NSPS (e.g., 0000 and 0000a) and the glycol circulation pump is electronic and also excluded from the definition of pneumatic pump in 60.5430a. Furthermore, the proposed project does not involve the installation of new compressors. As such, the project does not trigger a modification to the compressor station under 60.5365a(j).

National Emission Standards for Hazardous Air Pollutants

Part 63 NESHAP allowable emission limits are established on the basis of a maximum achievable control technology (MACT) determination for a particular major source. A HAP major source is defined as having potential emissions in excess of 25 tpy for total HAP and/or potential emissions in excess of 10 tpy for any individual HAP.

Note that Subpart HHH has specific major source applicability criteria (i.e., excluding engine emissions from the major source determination). The Curtisville Compressor Station is an Area (minor) source of HAP since its potential emissions of HAP are less than the 10/25 major source thresholds.

The only potentially applicable MACT standard for the proposed project is 40 CFR 63 Subpart HHH – Natural Gas Transmission and Storage Facilities. This MACT subpart applies to facilities which are major sources of HAP that transport or store natural gas prior to entering the transmission pipeline to end users as defined by 40 CFR §63.1271. The Curtisville Compressor Station is a natural gas transmission facility and is potentially subject to this subpart. However, the Curtisville Compressor Station is an area source based on the criteria of this MACT. Therefore, the requirements of this subpart do not apply.

West Virginia SIP Regulations

The Curtisville Compressor Station is potentially subject to regulations contained in the West Virginia Code of State Regulations, Chapter 45 (Code of State Regulations). The Code of State Regulations fall under two main categories, those regulations that are generally applicable (e.g., permitting requirements), and those that have specific applicability (e.g., PM standards for manufacturing equipment).

45 CSR 2: To Prevent and Control Particulate Air Pollution from Combustion of Fuel in Indirect Heat Exchangers

45 CSR 2 applies to fuel burning units, defined as equipment burning fuel "for the primary purpose of producing heat or power by indirect heat transfer". The reboiler is a fuel burning unit and therefore must comply with this regulation. Per 45 CSR 2-3, opacity of emissions from units shall not exceed 10 percent, based on a six-minute block average.

45 CSR 4: To Prevent and Control the Discharge of Air Pollutants into the Air Which Causes or Contributes to an Objectionable Odor

According to 45 CSR 4-3:

No person shall cause, suffer, allow or permit the discharge of air pollutants which cause or contribute to an objectionable odor at any location occupied by the public.

The Curtisville Compressor Station is generally subject to this requirement. However, due to the nature of the process at the station, production of objectionable odor from the compressor station during normal operation is unlikely.

45 CSR 6: Control of Air Pollution from the Combustion of Refuse

45 CSR 6 applies to activities involving incineration of refuse, defined as "the destruction of combustible refuse by burning in a furnace designed for that purpose. For the purposes of this rule, the destruction of any combustible liquid or gaseous material by burning in a flare or flare stack, thermal oxidizer or thermal catalytic oxidizer stack shall be considered incineration." The proposed dehydrator combustor is an incinerator and therefore must comply with this regulation.

Per 45 CSR 6-4.3, opacity of emissions from these units shall not exceed 20 percent, except as provided by 4.4. PM emissions from this unit will not exceed the levels calculated in accordance with 6-4.1 as demonstrated in the emission calculations in Attachment N.

45 CSR 10: To Prevent and Control Air Pollution from the Emission of Sulfur Oxides

This rule potentially applies to fuel burning units, including the glycol dehydration unit reboiler. Per 45 CSR 10-10.1, units rated less than 10 MMBtu/hr are exempt from the SO_2 emission limitations and testing, monitoring, recordkeeping, and reporting requirements of this rule. The reboiler is rated less than 10 MMBtu/hr and as such is exempt from this rule.

45 CSR 16: Standards of Performance for New Stationary Sources

45 CSR 16-1 incorporates the federal Clean Air Act (CAA) standards of performance for new stationary sources set forth in 40 CSR Part 60 by reference. As such, by complying with all applicable requirements of 40 CFR Part 60 at the Curtisville Compressor Station, Equitrans will be complying with 45 CSR 16.

45 CSR 17: To Prevent and Control Particulate 45 CSR 17: To Prevent and Control Particulate Matter Air Pollution from Materials Handling, Preparation, Storage and Other Sources of Fugitive Particulate Matter

According to 45 CSR 17-3.1:

No person shall cause, suffer, allow or permit fugitive particulate matter to be discharged beyond the boundary lines of the property lines of the property on which the discharge originates or at any public or residential location, which causes or contributes to statutory air pollution.

Due to the nature of the activities at the Curtisville Compressor Station it is unlikely that fugitive particulate matter emissions will be emitted under normal operating conditions. However, Equitrans will take measures to ensure any fugitive particulate matter emissions will not cross the property boundary should any such emissions occur.

45 CSR 34: Emissions Standards for Hazardous Air Pollutants

45 CSR 34-1 incorporates the federal Clean Air Act (CAA) national emissions standards for hazardous air pollutants (NESHAPs) as set forth in 40 CPR Parts 61 and 63 by reference. As such, by complying with all applicable requirements of 40 CFR Parts 61 and 63 at the Curtisville Compressor Station, Equitrans will be complying with 45 CSR 34.

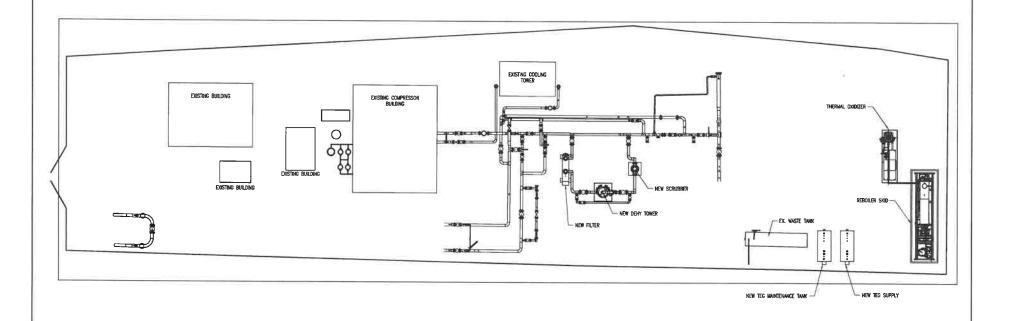
Non-Applicability of Other SIP Rules

An examination of the West Virginia SIP rules with respect to applicability at the Curtisville Compressor Station reveals many SIP regulations that do not apply or impose additional requirements on operations. Such SIP rules include those specific to a particular type of industrial operation that is categorically not applicable to the Curtisville Compressor Station.

ATTACHMENT E

Plot Plan





		REPERENCE DANIMES	Charles I Line Li	Mo.	DATE	REVISION	BY	DHK	APPD	160,	DATE	REVISION	BY	DE APPO	TO THE BEST OF MY KNOWLEDGE, ALL COMPONENTS OF THIS DRAWING ARE
ORAW	MIG HAMEE	DRAW	OR THUE	0	4/24/19	ISSUED FOR CONSTRUCTION	RSD	CM	-				-		DESIGNED IN ACCORDANCE WITH APPLICABLE GUIDELINES AND SPECIFICATIONS
	1		1		VA-2-1111									-	
	1	_	1												CLYDE MASTON 4/24/19
_	-		1												MECHANICAL DESIGN ENGINEER DATE
-	1		-	_			_	-		-					EE NAME 4/24/19
	1		1	_	_		\rightarrow	-	-	\vdash	_				ELECTRICAL DESIGNED DATE
	1		1						\vdash	ҥ			_	-	NOTE: ANY CHANGES TO THE DESIGN SHOWN ON THIS DRAWING MUST BE
	1		1											\rightarrow	APPROVED BY THE DESIGN ENGINEER.
File Path CAV	udi Working%Bysder	ns\Equitroos Transmission	NCurtieville CEVOre	swing Files Desig	n Files VPlant 30\CurtiseU	In CE\ Orthon\OWSe\C-W+CUR-1998-81.0vg		_					_		The second prompter.

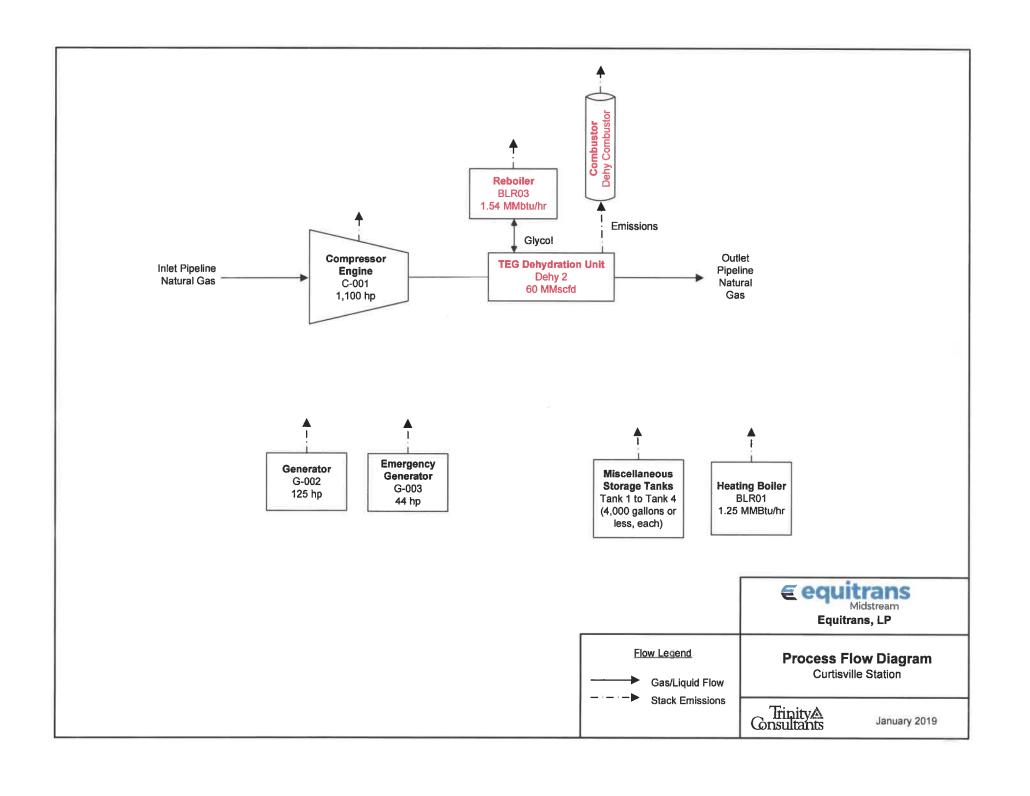
	EQT	•
ı	DESIGN ENGINEERING	l
	C14136	F

DRAWING TITLE.
CURTISVILLE COMPRESSOR STATION
MECHANICAL
PLOT PLAN – AIR PERMIT

C14136	FACILITY	STATE	IDENTIFICATION	SERRIS	SHEET	REVERN
3/32° = 1'-0°	C	W	CUR	1100	01	0

ATTACHMENT F

Detailed Process Flow Diagram



ATTACHMENT G

Process Description

Process Description

The Curtisville Compressor Station compresses and dehydrates natural gas and transports downstream along the pipeline system. Equitrans is submitting this application to replace the existing glycol dehydration unit, associated reboiler, and flare with a new 60 MMSCFD unit, associated reboiler (1.5 MMbtu/hr) and enclosed combustor for control. The remaining equipment at the facility will remain unchanged.

A process flow diagram is included as Attachment F.

ATTACHMENT I

Emission Units Table

Attachment I

Emission Units Table

(includes all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status)

Emission Point ID ²	Emission Unit Description	Year Installed/ Modified	Design Capacity	Type ³ and Date of Change	Control Device ⁴
C-001	Reciprocating Engine / Integral Compressor Clark, Model No. HRA8, Serial No. A-25900	1973	1,100 HP	Existing	None
G-002	Reciprocating Engine / Generator Kohler, Model No. 50 RZ-Ford	Mid 1990s	125 HP	Existing	None
G-003	Reciprocating Engine / Generator Kohler, Model No. 25REZG	2015	44 HP	Existing	None
Dehy Flare	TEG Dehydrator	1972	35 MMSCFD	Removed	Dehy Flare
Dehy Flare	Dehy Flare F1500 Model No. 44X1339	1990	0.08 MMBtu/hr	Removed	None
BLR01	Heating Boiler	1994	1.25 MMBtu/hr	Existing	None
BLR02	Dehydration Reboiler	1993	0.35 MMBtu/hr	Removed	None
Tank 1	Pipeline Condensate	1996	4,000 gallon	Existing	None
Tank 2	Triethylene Glycol	1996	500 gallon	Existing	None
Tank 3	Hydrate Inhibitor-Multi-chem MCMX5-2026	1996	330 gallon	Existing	None
Tank 4	Compressor Oil – CITGO Pacemaker 1035	1996	1,000 gallon	Existing	None
Dehy Combustor	TEG Dehydrator	2019	60 MMSCFD	New	Dehy Combustor
Dehy Combustor	Enclosed Combustor	2019	6.0 MMBtu/hr	New	None
BLR03	Dehydration Reboiler	2019	1.54 MMBtu/hr	New	None
	C-001 G-002 G-003 Dehy Flare Dehy Flare BLR01 BLR02 Tank 1 Tank 2 Tank 3 Tank 4 Dehy Combustor Dehy Combustor	Point ID2 Reciprocating Engine / Integral Compressor Clark, Model No. HRA8, Serial No. A-25900 Reciprocating Engine / Generator Kohler, Model No. 50 RZ-Ford Reciprocating Engine / Generator Kohler, Model No. 25REZG	Point ID2	Point ID2	Point ID2

¹ For Emission Units (or Sources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.
² For Emission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.
³ New, modification, removal
⁴ For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

Emission	Units	Table
	03	/2007

ATTACHMENT J

Emission Points Data Summary Sheet

Attachment J EMISSION POINTS DATA SUMMARY SHEET

						Т	able 1:	Emissions Da	ta								
Emission Point ID No. (Must match Emission Units Table & Plot Plan)	Emission Point Type ¹	Emission Unit Vented Through This Point (Must match Emission Units Table & Plot Plan)		Through This Point (Must match Emission		Air Pollution Control Device (Must match Emission Units Table & Plot Plan)		Vent Time for Emission Unit (chemical processes only)		All Regulated Pollutants - Chemical Name/CAS ³	Maximum Potential Uncontrolled Emissions ⁴		Maximum Potential Controlled Emissions ⁵		Form or Phase (At exit	Est. Method Used ⁶	Emission Concentration 7 (ppmv or mg/m ⁴)
		ID No.	Source	ID No.	Device Type	Short Term ²	Max (hr/yr)	(Speciate VOCs & HAPS)	lb/hr	ton/yr	lb/hr	ton/yr	conditions, Solid, Liquid or Gas/Vapor)				
C-001	Upward Vertical stack	C-001	Compressor Engine	NA	NA	NA	NA	NOx CO SO2 PM/PM10/PM2.5 VOC HAPs CO2e	28.94 3.52 0.01 0.44 1.10 0.73 1,069	126.77 15.44 0.02 1.94 4.80 3.18 4,678	28.94 3.52 0.01 0.44 1.10 0.73 1,069	126.77 15.44 0.02 1.94 4.80 3.18 4,678	Gas/Vapor	O _{A'B}			
G-002	Upward Vertical Stack	G-002	Generator Engine	NA	NA	NA	NA	NOx CO SO2 PM/PM10/PM2.5 VOC HAPs CO2e	0.70 1.18 <0.01 0.01 0.01 0.01 37	3.08 5.18 <0.01 0.03 0.04 0.04 163	0.70 1.18 <0.01 0.01 0.01 0.01 37	3.08 5.18 <0.01 0.03 0.04 0.04 163	Gas/Vapor	O ^{A,B}			
G-003	Upward Vertical Stack	G-003	Generator Engine	NA	NA	NA	NA	NOx CO SO2 PM/PM10/PM2.5 VOC HAPs CO2e	0.52 2.14 <0.01 0.01 0.52 0.01 48	0.13 0.54 <0.01 <0.01 0.13 <0.01	0.52 2.14 <0.01 0.01 0.52 0.01 48	0.13 0.54 <0.01 <0.01 0.13 <0.01 12	Gas/Vapor	O _{A,B}			
Dehy Combustor	Upward Vertical Stack	Dehy2	Dehy & Enclosed Combustor	Dehy Combust or	Enclosed Flare	NA	NA	NOx CO SO2 PM/PM10/PM2.5 VOC Methane CO2e HAP Benzene Toluene Ethlybenzene Xylene n-hexane	NA NA NA 14.74 25.47 638 7.78 0.91 1.57 2.33 2.78 0.18	NA NA NA 64.54 111.56 2,795 34.08 3.97 6.86 10.18 12.17 0.79	0.54 0.45 <0.01 0.04 0.32 0.52 717 0.16 0.02 0.03 0.05 0.06 <0.01	2.36 1.98 0.01 0.18 1.42 2.29 3,139 0.68 0.08 0.14 0.20 0.24 0.02	Gas/Vapor	OA.B.C			

BLR03	Upward Vertical Stack	BLR03	Dehy Reboiler	NA	NA	NA	NA	NOx CO SO2 PM/PM10/PM2.5 VOC HAPs CO2e	0.14 0.12 <0.01 0.01 0.01 <0.01 175	0.61 0.51 <0.01 0.05 0.03 0.01 765	0.14 0.12 <0.01 0.01 0.01 <0.01 175	0.61 0.51 <0.01 0.05 0.03 0.01 765	Gas/Vapor	O ^{A,B}	
BLR01	Upward Vertical Stack	BLR01	Heating Boiler	NA	NA	NA	NA	NOx CO SO2 PM/PM10/PM2.5 VOC HAPs CO2e	0.11 0.09 <0.01 0.01 0.01 <0.01 142	0.49 0.41 <0.01 0.04 0.03 0.01 621	0.11 0.09 <0.01 0.01 0.01 <0.01 142	0.49 0.41 <0.01 0.04 0.03 0.01 621	Gas/Vapor	O _{A,B}	

A- AP-42. See attachment N for additional details.

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit emissions are not typically considered to be fugitive and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugitive emission activities.

B- 40 CFR 98, Subpart C for natural gas fired combustion.

C- GRI-GLYCalc

¹ Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.

Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (ie., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).

List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. **DO NOT LIST** H₂, H₂O, N₂, O₃, and Noble Gases.

⁴ Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁵ Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmv) are used. If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m³) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO₂, use units of ppmv (See 45CSR10).

Attachment J EMISSION POINTS DATA SUMMARY SHEET

			Table 2: Rele	ase Paramet	er Data			
Emission Point ID No. (Must match Emission Units Table)	Inner Diameter (ft.)		Exit Gas		Emission Point El	evation (ft)	UTM Coordinates (km)	
		Temp. (ºF)	Volumetric Flow ¹ (acfm) at operating conditions	Velocity (fps)	Ground Level (Height above mean sea level)	Stack Height ² (Release height of emissions above ground level)	Northing	Easting

Give at operating conditions. Include inerts.
 Release height of emissions above ground level.

ATTACHMENT K

Fugitive Emissions Data Summary Sheet

LEAK SOURCE DATA SHEET

Source Category	Pollutant	Number of Source Components ¹	Number of Components Monitored by Frequency ²	Average Time to Repair (days) ³	Estimated Annual Emission Rate (lb/yr) ⁴
Pumps ⁵	light liquid VOC ^{6,7}				
	heavy liquid VOC ⁸				
	Non-VOC9				
Valves ¹⁰	Gas VOC	60	0		179
	Light Liquid VOC				
	Heavy Liquid VOC				
	Non-VOC				
Safety Relief Valves ¹¹	Gas VOC				
	Non VOC				
Open-ended Lines ¹²	voc	3	0		4
	Non-VOC				
Sampling Connections ¹³	voc	400	0		53
	Non-VOC				
Compressors	voc				
	Non-VOC				
Flanges	Voc	300	0		77
	Non-VOC				
Other	voc	40	0		233
	Non-VOC				

¹⁻¹³ See notes on the following page.

Notes for Leak Source Data Sheet

- For VOC sources include components on streams and equipment that contain greater than 10% w/w VOC, including feed streams, reaction/separation facilities, and product/by-product delivery lines. Do not include certain leakless equipment as defined below by category.
- 2. By monitoring frequency, give the number of sources routinely monitored for leaks, using a portable detection device that measures concentration in ppm. Do not include monitoring by visual or soap-bubble leak detection methods. "M/Q(M)/Q/SA/A/O" means the time period between inspections as follows:

Monthly/Quarterly, with Monthly follow-up of repaired leakers/Quarterly/Semi-annual/Annually/Other (specify time period)

If source category is not monitored, a single zero in the space will suffice. For example, if 50 gas-service valves are monitored quarterly, with monthly follow-up of those repaired, 75 are monitored semi-annually, and 50 are checked bimonthly (alternate months), with non checked at any other frequency, you would put in the category "valves, gas service:" 0/50/0/75/0/50 (bimonthly).

- 3. Give the average number of days, after a leak is discovered, that an attempt will be made to repair the leak.
- 4. Note the method used: MB material balance; EE engineering estimate; EPA emission factors established by EPA (cite document used); O other method, such as in-house emission factor (specify).
- 5. Do not include in the equipment count sealless pumps (canned motor or diaphragm) or those with enclosed venting to a control device. (Emissions from vented equipment should be included in the estimates given in the Emission Points Data Sheet.)
- 6. Volatile organic compounds (VOC) means the term as defined in 40 CFR □51.100 (s).
- 7. A light liquid is defined as a fluid with vapor pressure equal to or greater than 0.04 psi (0.3 Kpa) at 20°C. For mixtures, if 20% w/w or more of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20 °C, then the fluid is defined as a light liquid.
- 8. A heavy liquid is defined as a fluid with a vapor pressure less than 0.04 psi (0.3 Kpa) at 20°C. For mixtures, if less than 20% w/w of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20 °C, then the fluid is defined as a heavy liquid.
- 9. LIST CO, H₂S, mineral acids, NO, NO₂, SO₃, etc. DO NOT LIST CO₂, H₂, H₂O, N₂, O₂, and Noble Gases.
- 10. Include all process valves whether in-line or on an open-ended line such as sample, drain and purge valves. Do not include safety-relief valves, or leakless valves such as check, diaphragm, and bellows seal valves.
- 11. Do not include a safety-relief valve if there is a rupture disk in place upstream of the valve, or if the valve vents to a control device.
- 12 Open-ended lines include purge, drain and vent lines. Do not include sampling connections, or lines sealed by plugs, caps, blinds or second valves.
- 13. Do not include closed-purge sampling connections.

Attachment K

FUGITIVE EMISSIONS DATA SUMMARY SHEET

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not typically considered to be fugitive, and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET.

Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

	APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS
1.)	Will there be haul road activities?
	☐ Yes ☐ No (No change associated with this project)
	☐ If YES, then complete the HAUL ROAD EMISSIONS UNIT DATA SHEET.
2.)	Will there be Storage Piles?
	☐ Yes No
	$\ \square$ If YES, complete Table 1 of the NONMETALLIC MINERALS PROCESSING EMISSIONS UNIT DATA SHEET.
3.)	Will there be Liquid Loading/Unloading Operations?
	☑ Yes ☐ No (No change associated with this project)
	☐ If YES, complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET.
4.)	Will there be emissions of air pollutants from Wastewater Treatment Evaporation?
	☐ Yes
	☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
5.)	Will there be Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, open-ended valves, sampling connections, flanges, agitators, cooling towers, etc.)?
	⊠ Yes □ No
	$oxed{\boxtimes}$ If YES, complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS UNIT DATA SHEET.
6.)	Will there be General Clean-up VOC Operations?
	☐ Yes
	☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
7.)	Will there be any other activities that generate fugitive emissions?
	☐ Yes
	☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form.
If yo	bu answered "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions nmary."

FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants - Chemical Name/CAS1		Potential Emissions ²	Maximum Controlled E	Est. Method		
	J. J	lb/hr	ton/yr	lb/hr	ton/yr	Used 4	
Haul Road/Road Dust Emissions Paved Haul Roads	NA		-				
Unpaved Haul Roads	NA						
Storage Pile Emissions	NA					 	
Road Packing Emissions	VOC HAP		0.29 <0.01		0.29 <0.01	OB	
Wastewater Treatment Evaporation & Operations	NA			757			
Equipment Leaks	VOC HAP	N/A	0.27 <0.01	N/A	0.27 <0.01	O ^A	
General Clean-up VOC Emissions	NA						
Other – Blowdowns, ESD and Pigging Events	VOC HAP	N/A	0.31 <0.01	N/A	0.31 <0.01	ОВ	

A – Oil and Gas Production Operations Average Emission Factors, Protocol for Equipment Leak Emission Estimates, EPA 453/R-95-017, Table 2-4, November 1995, 40 CFR 98 Subpart W, and mass balance.

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B - Mass Balance

¹ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. DO NOT LIST H₂, H₂O, N₂, O₂, and Noble Gases.

² Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

³ Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁴ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

ATTACHMENT L

Emissions Unit Data Sheet

Attachment L EMISSIONS UNIT DATA SHEET GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form): DEHY2

γ.γ
Name or type and model of proposed affected source:
60 MMSCFD dehydration unit with 1.54 MMBtu/hr heat input rated reboiler
 On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.
3. Name(s) and maximum amount of proposed process material(s) charged per hour:
60 million standard cubic feet per day of natural gas
^
4. Name(s) and maximum amount of proposed material(s) produced per hour:
Does not produce a material – removes water from wet natural gas
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:
External combustion of natural gas in reboiler
* The identification number which appears here must correspond to the air pollution control device

^{*} The identification number which appears here must correspond to the air pollution control device identification number appearing on the List Form.

6. Combustion Data (if applic	able):							
(a) Type and amount in ap	propriate units of fuel(s) to be bu	ırned:						
Reboiler - Natural gas – 1,38	2 scfh							
(b) Chemical analysis of prand ash:	roposed fuel(s), excluding coal, in	ncluding maximum percent sulfur						
Natural gas with negligible H	I_2S and ash content.							
(c) Theoretical combustion	air requirement (ACF/unit of fue	el):						
Unknown @	°F and	psia.						
(d) Percent excess air: \(\text{I}	Jnknown	_						
(e) Type and BTU/hr of bu	rners and all other firing equipme	ent planned to be used:						
natural gas fired external com	natural gas fired external combustion heater – 1.54 MMbtu/hr input rating							
(f) If coal is proposed as a coal as it will be fired:	source of fuel, identify supplier	and seams and give sizing of the						
NA								
(g) Proposed maximum de	sign heat input: 1.	54 × 10 ⁶ BTU/hr.						
7. Projected operating schedu	ıle:	v						
Hours/Day 24	Days/Week 7	Weeks/Year 52						

8.	Projected amount of polluta	ants that would be a	emitted fro	om this affected source if no control
	devices were used:	and that would be t	onintou ne	on this ancolog source if no control
@) Unknown	°F and		psia
a.	NO _X	0.14	lb/hr	grains/ACF
b.	SO ₂	<0.01	lb/hr	grains/ACF
C.	СО	0.12	lb/hr	grains/ACF
d.	PM ₁₀	0.01	lb/hr	grains/ACF
e.	Hydrocarbons		lb/hr	grains/ACF
f.	VOCs	14.74	lb/hr	grains/ACF
g.	Pb		lb/hr	grains/ACF
h.	Specify other(s)			5
	HAPs	7.78	lb/hr	grains/ACF
	Benzene	0.91	lb/hr	grains/ACF
	Toluene	1.57	lb/hr	grains/ACF
	Ethylbenzene	2.33	lb/hr	grains/ACF
	Xylene	2.78	lb/hr	grains/ACF
	n-hexane	0.18	lb/hr	grains/ACF

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

⁽²⁾ Complete the Emission Points Data Sheet.

	and reporting in order to demonstrate compliance Please propose testing in order to demonstrate
MONITORING	RECORDKEEPING
Throughput of wet natural gas. Operating parameters of dehydration unit for GLYCalc (temperature, pressure, glycol flow rate)	Maintain records of the times and duration of all periods which the pilot flame was absent
Conduct visual inspections one per month confirming the pilot is lit	
DEDODTINO	
REPORTING None.	TESTING
	E PROCESS PARAMETERS AND RANGES THAT ARE STRATE COMPLIANCE WITH THE OPERATION OF THIS CONTROL DEVICE.
RECORDKEEPING. PLEASE DESCRIBE THE PROPMONITORING.	OSED RECORDKEEPING THAT WILL ACCOMPANY THE
REPORTING. PLEASE DESCRIBE THE PRORECORDKEEPING.	POSED FREQUENCY OF REPORTING OF THE
TESTING. PLEASE DESCRIBE ANY PROPOSED EMISPOLLUTION CONTROL DEVICE.	SSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR
10. Describe all operating ranges and mainter maintain warranty	nance procedures required by Manufacturer to

ATTACHMENT M

Air Pollution Control Device Sheet

Attachment M Air Pollution Control Device Sheet

(FLARE SYSTEM)

Control Device ID No. (must match Emission Units Table): Dehy Combustor

Equipment Information

1. Manufacturer: Envirotherm (or similar) Elevated flare Method: Model No. ETI-DVC-36 (or similar) Ground flare Other Describe Enclosed Flare 3. Provide diagram(s) of unit describing capture system with duct arrangement and size of duct, air volume, capacity, horsepower of movers. If applicable, state hood face velocity and hood collection efficiency. 4. Method of system used: ☐ Steam-assisted ☐ Air-assisted ☐ Pressure-assisted 5. Maximum capacity of flare: 6. Dimensions of stack: scf/min Diameter 3 ft. scf/hr Height 20 ft. 7. Estimated combustion efficiency: 8. Fuel used in burners: (Waste gas destruction efficiency) Natural Gas > 98 Estimated: % ☐ Fuel Oil, Number > 98 % Minimum guaranteed: Other, Specify: 11. Describe method of controlling flame: 9. Number of burners: One (1) Rating: 6 MMBTU/hr 10. Will preheat be used? ⊠ No 14. Natural gas flow rate to flare pilot flame per pilot light: 20 ft Flare height: scf/min 13. Flare tip inside diameter: 28 inches ft NA scf/hr 15. Number of pilot lights: One (1) Burner 16. Will automatic re-ignition be used? ⊠ Yes 2 MMBTU/hr □ No Total 17. If automatic re-ignition will be used, describe the method: □ No 18. Is pilot flame equipped with a monitor? ✓ Yes If yes, what type? Thermocouple ☐ Infra-Red ☐ Ultra Violet ☐ Camera with monitoring control room Other, Describe: 19. Hours of unit operation per year: 8760

Steam Injection

			Ottouiii .	injourie	011		
20.	. Will steam injection be use	d? 🗌 Yes	⊠ No	21. S	Steam pressure		PSIG
					finimum Expected:		
				D	esign Maximum:		
22.	Total Steam flow rate:		LB/hr	23. T	emperature:		°F
24.	Velocity		ft/sec	25. N	lumber of jet streams		
26.	Diameter of steam jets:		in		Design basis for steam	iniected:	
	·					•	n/LB hydrocarbon
28.	How will steam flow be con	trolled if steam i	injection is	used?	?		
	Cha	aracteristics of	the Wast	e Gae	Stream to be Burne		
29.		Quan		- Cus	Quantity		
	Name	Grains of Ha			(LB/hr, ft³/hr, etc)	Soi	urce of Material
		See a	ttached e	missior	ns calculations		
	-						
						+	
						+	
20	Estimate total combustible t	de flore.		0.00 (5	OLVI-\ LD#		
30.			э	o.∠8 (ĭĭ	rom GLYcalc) LB/i		
21	(Maximum mass flow rate of		-4		scfn		
ادا	Estimated total flow rate to	nare including in	iateriais to	o be bu	ırned, carrier gases, a	uxillary tu	el, etc.: 8,897 scfn
32	Give composition of carrier	uases.					
~~	ONE composition of carrier	gases.					
				34. Id	entify and describe all	auxiliary	fuels to be burned.
33.	Temperature of emission stress >100	ream: °F					BTU/scf
	Heating value of emission s	-					BTU/scf
)57 BTU/ft ³					BTU/scf
	Mean molecular weight of e MW = lb/lb-mole	mission stream:					BTU/scf
							BTU/scf
35.	Temperature of flare gas:	1450-1600 °F		36. Fla	are gas flow rate:	660	scf/min
37.	Flare gas heat content: 8 to	1,057 BTU/ft	3	38. Fla	are gas exit velocity:	9.34 ft/se	ec
39.	Maximum rate during emerg	gency for one ma	ajor piece	of equ	ipment or process uni	t:	scf/min
	Maximum rate during emerg						BTU/min
41.	Describe any air pollution or reheating, gas humidification	control device in n):	nlet and o	utlet ga	as conditioning proce	sses (e.g	., gas cooling, gas
42.	Describe the collection mate	erial disposal sy	stem:				
43.	Have you included Flare Co	ontrol Device in	the Emis	sions P	Points Data Summary	Sheet?	

Please propose mo operating paramete limits.	ring, Recordkeeping, Reporting, onitoring, recordkeeping, and report ers. Please propose testing in orde	and Testing ting in order to demonstrate compliance with the proposeder to demonstrate compliance with the proposed emissions
MONITORING: Presence of pilot	t (temperature)	RECORDKEEPING: Maintain records of the times and duration of all periods where the pilot flame was absent
		Maintain records of visible emission opacity tests
REPORTING: None		TESTING: Conduct a Method 22 opacity test as required
MONITORING:	Please list and describe the promonitored in order to demonstrate or air control device.	ocess parameters and ranges that are proposed to be ecompliance with the operation of this process equipment
RECORDKEEPING: REPORTING:	Please describe the proposed red	cordkeeping that will accompany the monitoring. nissions testing for this process equipment on air pollution
TESTING:		nissions testing for this process equipment on air pollution
45. Manufacturer's Gua VOC – 100% HAP – 100%	aranteed Capture Efficiency for eac	ch air pollutant.
46. Manufacturer's Gua VOC – 98% HAP – 98%	aranteed Control Efficiency for each	h air pollutant.
VOC – 98%	aranteed Control Efficiency for eacl	h air pollutant.
VOC – 98% HAP – 98%		
VOC – 98% HAP – 98%		h air pollutant.
VOC – 98% HAP – 98%		



Flare Stacks - Thermal Oxidizers - Burners & Controls

PROPOSAL FOR Equitrans – Curtisville DEHY 36-DVC

Customer:

Equitrans Midstream

Attn:

Clyde Maston

(304) 543-7256

Prepared By:

Chuck Stephenson

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Proposal Number

18186 Rev 0



Technical Summary

Standard Design Conditions: Curtisville DEHY 650 MMSCFD

Process Inlet Stream: Based on GRI-Gly Calc Output:

Overhea	Overhead Still 4" Inlet							
Inlet Temperature:	212°F							
Inlet Pressure:	≥ 2" WC							
Flow Rate:	8450 SCFH							
Net Heat Release:	8 BTU/FT^3							
Flash Gas 1" Inlet								
Inlet Temperature: 130°F								
Inlet Pressure:	35 PISG							
Flow Rate:	447 SCFH							
Net Heat Release:	1057 BTU/FT^3							
36" Combu	ustion Chamber							
Exit Diameter:	28 IN I.D.							
Mass Flow @ 1450°F:	143,629 ACFH							
Exit Velocity:	9.34 FT/SEC							
DVC's Max Heat Design Load:	6 MMBTU/HR							
Designed Heat Load:	0.6 MMBTU/HR							
Combustion Chamber Temp:	1450 – 1600 °F							
Destruction Efficiency:	≥98.0%							
Residence Time:	≥1.8 Sec.							

Site Conditions						
Wind Speed: 105 MPH						
Seismic Zone:	1					
Elevation:	1,200 FASL					
Humidity:	High					

Utiilities							
	1000 SCFH - Natural Gas						
Gas Service Required for Burner:	intermittent use, only on when						
	temperature < 1450 °F						
Electrical Service Required:	24 VDC, 5 Amps						
Gas Consumption at Start-up:	1.0 MMBtu/hr						
Gas Consumption under load:	≤ 400 SCFH, Dependant on BTU						
Gas Consumption under load.	value of waste stream						

ATTACHMENT N

Supporting Emission Calculations

Equitrans, LP Curtisville Station R13 Permit Application

			F	acility-Wide En	nissions Summa	ry					
	Clark Compressor Engine	Kohler 50 RZ Generator	Kohler 25 REZG Generator	TEG Dehy Unit	Dehydration Combustor	Dehy Reboiler	Heating Boiler				
Emission Unit ID	C-001	G-002	G-003	Dehy2	Dehy Combustor	BLR03	BLR01	Fugitives	Total Potential Emissions	Project Increase Emissions	
Fuel Type	Natural Gas	Natural Gas	Natural Gas		Natural Gas	Natural Gas	Natural Gas	& Blowdowns			
Capacity	1,100	125	44	60	6.00	1.54	1.25				
Unit	HP	HP	НР	MMSCFD	MMBtu/hr	MMBtu/hr	MMBtu/hr				
Operating Hours (hrs)	8,760	8,760	500	8,760	8,760	8,760	8,760	8,760			
# of Emission Units	1	1	1	1	1	1	1	N/A			
Pollutant	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	
PM ₁₀	1.94	0.03	2.0E-03		0.18	0.05	0.04		2.23	0.23	
PM _{2.5}	1.94	0.03	2.0E-03		0.18	0.05	0.04	-	2.23	0.23	
SO _X	0,02	8,2E-04	6,0E-05		0.01	3.6E-03	2.9E-03		0.05	0.02	
СО	15.44	5.18	0.54		1.98	0.51	0.41	-	24.06	2.49	
NO _X	126.77	3.08	0.13		2.36	0.61	0.49		133.43	2.96	
VOC	4.80	0.04	0.13	1.29	1.3E-01	0.03	0.03	0.87	7.32	1.45	
CO_2	4,678	163	12	6.25	3,074	765	621	0.08	9,318	3,845	
CH ₄	0.09	3.1E-03	2.2E-04	2.23	5.8E-02	1.4E-02	0.01	16,23	19	2.30	
N ₂ O	0.01	3.1E-04	2.2E-05		5.8E-03	1.4E-03	1.2E-03		0.02	0.01	
CO ₂ e ¹	4,683	163	12	62	3,077	765	621	406	9,789	3,905	
Formaldehyde	2.21	0.03	2.1E-03			4.5E-04	3.7E-04		2.24	0.00	
Benzene	0.08	2.2E-03	1.6E-04	0.08		1.3E-05	1.0E-05		0.16	0.08	
Toluene	0.04	7.8E-04	5.7E-05	0.14		2.1E-05	1.7E-05		0.18	0.14	
Ethylbenzene	4.3E-03	3.5E-05	2.5E-06	0.20					0.21	0.20	
Xylene	0.01	2.7E-04	2.0E-05	0.24	-				0.25	0.24	
n-Hexane	0.02			0.02	-	1.1E-02	0.01		0.05	0.03	
Total HAPs (including HCHO)	3,18	0.04	3.0E-03	0.68	-	1.1E-02	0.01	0.01	3.94	0.69	

^{1.} Conversion to $\rm CO_2e$ based on $\rm CH_4$ GWP = 25 and $\rm N_2O$ GWP = 298, per 40 CFR 98. 2. VOC includes Formaldehyde.

Equitrans, LP
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Dehydrator Emission Calculations

			Regen				Flash Tank					Potential To Emit*				
	Uncontrolled Emissions			Controlled Emissions		Unco	Uncontrolled Emissions		Controlled Emissions			Uncontrolled		Controlled		
Pollutant	(lbs/hr)	(lbs/day)	(tons/yr)	(lbs/hr)	(lbs/day)	(tons/yr)	(lbs/hr)	(lbs/day)	(tons/yr)	(lbs/hr)	(lbs/day)	(tons/yr)	(lbs/hr)	(tons/yr)	(lbs/hr)	(tons/vr
Carbon Dioxide	0.5220	12.5280	2.2864	0.5220	12.5280	2,2864	0.6670	16,008	2.9215	0.6670	16,008	2.9215	1,43	6.25	1,43	6.25
Methane	10.4194	250.0650	45,6368	0,2084	5.0010	0,9127	10.8052	259.325	47.3269	0.2161	5.187	0.9465	25.47	111.56	0.51	2.23
Ethane	4,3923	105.4160	19,2384	0.0878	2.1080	0.3848	9.0042	216,101	39.4384	0.1801	4,322	0.7888	16.08	70.41	0.32	1.41
Рторапе	0.9510	22.8240	4.1654	0.0190	0.4560	0.0833	1,5443	37.062	6.7639	0.0309	0.741	0.1353	2.99	13.12	0.06	0.26
Isobutane	0.2467	5,9210	1.0806	0.0049	0.1180	0.0216	0.3063	7.350	1.3414	0.0061	0.147	0.0268	0.66	2.91	0.01	0.06
n-Butane	0.4324	10,3770	1.8937	0,0086	0.2080	0.0379	0.4366	10,478	1.9122	0.0087	0,210	0.0382	1.04	4.57	0.02	0.00
Isopentane	0.1599	3,8380	0.7004	0.0032	0.0770	0.0140	0.1426	3.422	0.6245	0.0029	0.068	0.0125	0.36	1.59	0.02	0.03
n-Pentane	0.1134	2.7230	0.4969	0.0023	0.0540	0,0099	0.0834	2,001	0,3651	0.0017	0.040	0.0073	0.24	1.03	0.00	0.03
Cyclopentane	0,0593	1.4240	0.2599	0.0012	0.0280	0.0052	0.0109	0.262	0.0478	0.0002	0.005	0.0010	0.08	0,37	0.00	0.02
n-Hexane	0.1056	2.5340	0.4624	0.0021	0.0510	0.0092	0.0441	1.058	0.1930	0.0009	0.021	0.0039	0.18	0.79	0.00	0.02
Cyclohexane	0.1549	3.7190	0.6787	0.0031	0.0740	0.0136	0.0157	0.376	0.0686	0.0003	0.008	0.0014	0.20	0.90	0.00	0.02
Other Hexanes	0.2807	6,7360	1.2294	0,0056	0.1350	0.0246	0,1520	3,647	0,6656	0.0030	0.073	0.0133	0.52	2.27	0.01	0.02
Heptanes	0.3125	7.5010	1.3689	0.0063	0.1500	0.0274	0.0636	1,527	0.2787	0.0013	0.031	0.0056	0.45	1.98	0.01	0.03
Methylcyclohexane	0.2266	5.4380	0.9925	0.0045	0.1090	0.0198	0.0179	0.430	0.0784	0.0004	0.009	0.0016	0.29	1.29	0.01	0.03
2,2,4-Trimethylpentane	0.0152	0.3650	0.0665	0.0003	0,0070	0.0013	0,0060	0.143	0.0262	0.0001	0.003	0.0005	0.03	0.11	0.00	0.00
Benzene	0.7443	17.8640	3.2602	0.0149	0.3570	0.0652	0.0118	0,282	0.0515	0.0002	0.006	0.0010	0.91	3.97	0.02	0.08
Toluene	1,2918	31.0030	5.6580	0.0258	0,6200	0.1132	0.0130	0,312	0.0570	0.0003	0.006	0.0011	1.57	6.86	0.02	0.08
Ethylbenzene	1.9264	46,2340	8,4378	0.0385	0.9250	0,1688	0.0111	0.267	0.0488	0.0002	0.005	0.0010	2.33	10.18	0.05	0.14
Xylenes	2.3050	55,3210	10.0961	0.0461	1.1060	0.2019	0.0095	0.227	0.0415	0.0002	0.005	0.0008	2.78	12.17	0.05	0.24
C8 + Heavier Hydrocarbons	0,0839	2.0130	0,3674	0.0017	0.0400	0.0073	0.0016	0.039	0.0071	<0.0001	0.001	0.0001	0.10	0.45	<0.0001	0.01
Total Emissions	24,2215	581,3150	106.0900	0.4844	11.6260	2.1218	22.6796	544.310	99.3366	0.4536	10,886	1.9867				
Total Hydrocarbon Emission	24,2215	581,3150	106,0900	0.4844	11.6260	2.1218	22.6796	544.310	99.3366	0.4536	10.886	1.9867	56.28	246.51	1.13	4.93
Total VOC Emissions	9.4098	225,8350	41.2148	0.1882	4.5170	0.8243	2.8702	68.884	12.5713	0.4536	1.378	0.2514	56.28	246.51	1.13	4.93
Total HAP Emissions	6.3884	153.3210	27.9810	0.1278	3.0660	0.5596	0.0954	2.290	0.4180	0.0374	0.046	0,2514	14.74	64.54	0.29	1,29
GHG Emissions (CO2e)	261,0070		1143.2064	5.7320	137.5530	25,1039	270,7970	6499.133	1186.0940	6.0695	145,683	26.5840	7.78 638,16	34.08 2795.16	0.16 14.16	0,68 62,03

^{*} As calculated using GRI-GLYCalc 4.0, at a worst-case emissions scenario of design rated dry gas flowrate of 60 MMscf/day, tower operating conditions of T and P of 45°F and 650 psig (respectively), flash tank conditions of T and P of 135°F and 35 psig (respectively), and maximum glycol pump rate of 10 gpm. The GLYCalc run uses the most recent extended gas analysis available for the station, and 0.0005% for all NIL compounds reported on extended gas analysis.

^{*} Potential to emit is calculated by adding 20% compliance margin to GRI-GLYCalc results to account for variation in the extended gas analysi

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Dehydrator Flare Emission Calculations

Source Designation:	
Manufacturer:	Envirotherm
Model:	DVC-36
Year Installed	2019
Fuel Used:	Natural Gas
Higher Heating Value (HHV) (Btu/scf):	1,114
Heat Input (MMBtu/hr)	6.00
Fuel Consumption (mmscf/hr):	5,39E-03
Potential Annual Hours of Operation (hr/yr):	8,760

Criteria and Manufacturer Specific Pollutant Emission Rates:

	Emission Factor		Potential Emissions	
Pollutant	(lb/MMscf)*	(lb/hr) ^b	(tons/yr)°	
NO _x	100	0.54	2,36	
СО	84	0.45	1.98	
SO ₂	0,6	3.2E-03	1.4E-02	
PM Total	7.6	4.1E-02	1.8E-01	
PM Condensable	5.7	3.1E-02	1.3E-01	
PM ₁₀ (Filterable)	1.9	1.0E-02	4.5E-02	
PM _{2.5} (Filterable)	1.9	1.0E-02	4.5E-02	
voc	5.5	3.0E-02	1.3E-01	
CO2d (Natural Gas Firing)	116.98	701.86	3074.13	
CH ₄ ^d (Natural Gas Firing)	0.002	1.3E-02	5.8E-02	
N ₂ O ^d (Natural Gas Firing)	0.0002	1.3E-03	5.8E-03	

^a Emission factors from AP-42 Section 1.4 "Natural Gas Combustion" Tables 1.4-1, 1.4-2, & 1.4-3

45-6-4 Emission Standard Calculation:

Emissions (lb/hr) =		w.
5.43	56.28 lb	hr
	hr	2000 lb
=		0.15 lb/hr

^b Emission Rate (lb/hr) = Rated Capacity (MMscf/hr) × Emission Factor (lb/MMscf).

[°] Annual Emissions (tons/yr), Octobrical = (lb/hr), Emissions × (Maximum Allowable Operating Hours, 8760 hr/yr) × (1 ton/2000 lb).

^d GHG Emission factors from Tables C-1 and C-2, 40 CFR 98, Subpart C and are in units of lb/MMBtu.

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Dehydration Reboiler Calculations

Source Designation:	
Year Installed	2019
Fuel Used:	Natural Gas
Higher Heating Value (HHV) (Btu/scf):	1,114
Heat Input (MMBtu/hr)	1.54
Fuel Consumption (mmscf/hr):	1.38E-03
Fuel Consumption (mmscf/yr):	12.11
Potential Annual Hours of Operation (hr/yr):	8,760

Criteria and Manufacturer Specific Pollutant Emission Rates:

	Emission Factor	Potential Emissions	
Pollutant	(lb/MMscf) ^a	(lb/hr) ^b	(tons/yr) ^c
NO _x	100	0.14	0.61
CO	84	0.12	0,51
SO ₂	0.6	8.3E-04	3.6E-03
PM Total	7.6	1.1E-02	0.05
PM Condensable	5.7	7.9E-03	0.03
PM ₁₀ (Filterable)	1.9	2.6E-03	1.2E-02
PM _{2.5} (Filterable)	1.9	2.6E-03	1.2E-02
VOC	5.5	7.6E-03	0.03
CO2d (Natural Gas Firing)	126,262	174.55	764.51
CH4d (Natural Gas Firing)	2.4	3.3E-03	1.4E-02
N ₂ O ^d (Natural Gas Firing)	0.24	3.3E-04	1.4E-03

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Dehydration Reboiler Calculations

Hazardous Air Pollutant (HAP) Potential Emissions:

	Emission Factor	Potential Emissions		
Pollutant	(lb/MMscf) ^a	(lb/hr) ^b	(tons/yr) ^c	
HAPs:				
3-Methylchloranthrene	1.80E-06	2.49E-09	1.09E-08	
7,12-Dimethylbenz(a)anthracene	1.60E-05	2.21E-08	9.69E-08	
Acenaphthene	1.80E-06	2.49E-09	1.09E-08	
Acenaphthylene	1.80E-06	2.49E-09	1,09E-08	
Anthracene	2,40E-06	3,32E-09	1,45E-08	
Benz(a)anthracene	1.80E-06	2,49E-09	1.09E-08	
Benzene	2.10E-03	2.90E-06	1.27E-05	
Benzo(a)pyrene	1,20E-06	1.66E-09	7.27E-09	
Benzo(b)fluoranthene	1.80E-06	2.49E-09	1.09E-08	
Benzo(g,h,i)perylene	1.20E-06	1,66E-09	7.27E-09	
Benzo(k)fluoranthene	1.80E-06	2.49E-09	1.09E-08	
Chrysene	1.80E-06	2.49E-09	1.09E-08	
Dibenzo(a,h) anthracene	1.20E-06	1.66E-09	7.27E-09	
Dichlorobenzene	1.20E-03	1.66E-06	7.27E-06	
Fluoranthene	3.00E-06	4.15E-09	1,82E-08	
Fluorene	2.80E-06	3.87E-09	1.70E-08	
Formaldehyde	7.50E-02	1.04E-04	4.54E-04	
Hexane	1.80E+00	2.49E-03	1.09E-02	
Indo(1,2,3-cd)pyrene	1,80E-06	2.49E-09	1.09E-08	
Phenanthrene	1.70E-05	2,35E-08	1.03E-07	
Pyrene	5.00E-06	6,91E-09	3,03E-08	
Toluene	3.40E-03	4.70E-06	2,06E-05	
Arsenic	2.00E-04	2.76E-07	1.21E-06	
Beryllium	1.20E-05	1.66E-08	7.27E-08	
Cadmium	1.10E-03	1,52E-06	6,66E-06	
Chromium	1.40E-03	1.94E-06	8.48E-06	
Cobalt	8.40E-05	1.16E-07	5.09E-07	
Lead	5.00E-04	6.91E-07	3.03E-06	
Manganese	3.80E-04	5.25E-07	2.30E-06	
Mercury	2.60E-04	3.59E-07	1.57E-06	
Nickel	2.10E-03	2.90E-06	1.27E-05	
Selenium	2.40E-05	3.32E-08	1.45E-07	
		-		
Polycyclic Organic Matter:	1			
Methylnaphthalene (2-)	2,40E-05	3.32E-08	1.45E-07	
Naphthalene	6.10E-04	8.43E-07	3.69E-06	
Total HAP		2.61E-03	1,14E-02	

^a Emission factors from AP-42 Section 1.4 "Natural Gas Combustion" Tables 1.4-1, 1.4-2, & 1.4-3

^b Emission Rate (lb/hr) = Rated Capacity (MMscf/hr) × Emission Factor (lb/MMscf).

⁶ Annual Emissions (tons/yr)_{Fotential} = (lb/hr)_{Emissions} × (Maximum Allowable Operating Hours, 8760 hr/yr) × (1 ton/2000 lb).

^d GHG Emission factors from Tables C-1 and C-2, 40 CFR 98, Subpart C.

GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES

Case Name: EQT - Curtisville Dehy PTE

File Name: Z:\Client\EQT Corporation\West Virginia\Curtisville\Projects\183901.0271 Dehy

Replacement\03 Deliverables\2019-0122 Revised Application\Attach N - Emission

Calculations\2019-0122 Curtisville_DehyCalcs_v1.1.ddf
Date: January 22, 2019

DESCRIPTION:

Description: Gas analysis sample date: 9/30

Annual Hours of Operation: 8760.0 hours/yr

WET GAS:

Temperature: 45.00 deg. F Pressure: 650.00 psig

Wet Gas Water Content: Saturated

Component	Conc. (vol %)
Carbon Dioxide	0.1490
Nitrogen	0.3870
Methane	87.2360
Ethane	11.1700
Propane	0.8080
Isobutane	0.0870
n-Butane	0.0990
Isopentane	0.0250
n-Pentane	0.0120
Cyclopentane	0.0010
n-Hexane	0.0040
Cyclohexane	0.0010
Other Hexanes	0.0160
Heptanes	0.0040
Methylcyclohexane	0.0010
2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene Xylenes	0.0005 0.0005 0.0005 0.0005
C8+ Heavies	0.0005

DRY GAS:

Flow Rate: 60.0 MMSCF/day Water Content: 7.0 lbs. H2O/N

7.0 lbs. H20/MMSCF

LEAN GLYCOL:

Glycol Type: TEG

Water Content: 1.0 wt% Flow Rate: 10.0 gpm

1.0 wt% H2O

Page: 2 PUMP: ------Glycol Pump Type: Electric/Pneumatic FLASH TANK: Flash Control: Combustion device Flash Control Efficiency: 98.00 % Temperature: 135.0 deg. F Pressure: 35.0 psig

STRIPPING GAS:

Source of Gas: Dry Gas

Gas Flow Rate: 4.400 scfm

REGENERATOR OVERHEADS CONTROL DEVICE:

Control Device: Combustion Device

Destruction Efficiency: 98.0 %
Excess Oxygen: 2.0 %
Ambient Air Temperature: 60.0 deg. F

GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: EQT - Curtisville Dehy PTE

File Name: Z:\Client\EQT Corporation\West Virginia\Curtisville\Projects\183901.0271 Dehy

Replacement\03 Deliverables\2019-0122 Revised Application\Attach N - Emission

Calculations\2019-0122 Curtisville_DehyCalcs_v1.1.ddf Date: January 22, 2019

DESCRIPTION:

Description: Gas analysis sample date: 9/30 Annual Hours of Operation: 8760.0 hours/yr

EMISSIONS REPORTS:

CONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.2084	5.001	0.9127
Ethane	0.0878	2.108	0.3848
Propane	0.0190	0.456	0.0833
Isobutane	0.0049	0.118	0.0216
n-Butane	0.0086	0.208	0.0379
Isopentane	0.0032	0.077	0.0140
n-Pentane	0.0023	0.054	0.0099
Cyclopentane	0.0012	0.028	0.0052
n-Hexane	0.0021	0.051	0.0092
Cyclohexane	0.0031	0.074	0.0136
Other Hexanes	0.0056	0.135	0.0246
Heptanes	0.0063	0.150	0.0274
Methylcyclohexane	0.0045	0.109	0.0198
2,2,4-Trimethylpentane	0.0003	0.007	0.0013
Benzene	0.0149	0.357	0.0652
Toluene	0.0258	0.620	0.1132
Ethylbenzene	0.0385	0.925	0.1688
Xylenes	0.0461	1.106	0.2019
C8+ Heavies	0.0017	0.040	0.0073
Total Emissions	0.4844	11.626	2.1218
Total Hydrocarbon Emissions	0.4844	11.626	2.1218
Total VOC Emissions	0.1882	4.517	0.8243
Total HAP Emissions	0.1278	3.066	0.5596
Total BTEX Emissions	0.1254	3.008	0.5490

UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	10.4194	250.065	45.6368
Ethane	4.3923	105.416	19.2384
Propane	0.9510	22.824	4.1654
Isobutane	0.2467	5.921	1.0806
n-Butane	0.4324	10.377	1.8937
Isopentane	0.1599	3.838	0.7004
n-Pentane	0.1134	2.723	0.4969
Cyclopentane	0.0593	1.424	0.2599

n-Hexane Cyclohexane	0.1056 0.1549	2.534 3.719	Page: 2 0.4624 0.6787
Other Hexanes Heptanes Methylcyclohexane 2,2,4-Trimethylpentane Benzene	0.2807	6.736	1.2294
	0.3125	7.501	1.3689
	0.2266	5.438	0.9925
	0.0152	0.365	0.0665
	0.7443	17.864	3.2602
Toluene	1.2918	31.003	5.6580
Ethylbenzene	1.9264	46.234	8.4378
Xylenes	2.3050	55.321	10.0961
C8+ Heavies	0.0839	2.013	0.3674
Total Emissions	24.2215	581.315	106.0900
Total Hydrocarbon Emissions	24.2215	581.315	106.0900
Total VOC Emissions	9.4098	225.835	41.2148
Total HAP Emissions	6.3884	153.321	27.9810
Total BTEX Emissions	6.2676	150.422	27.4521

FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.2161	5.187	0.9465
Ethane	0.1801	4.322	0.7888
Propane	0.0309	0.741	0.1353
Isobutane	0.0061	0.147	0.0268
n-Butane	0.0087	0.210	0.0382
Isopentane	0.0029	0.068	0.0125
n-Pentane	0.0017	0.040	0.0073
Cyclopentane	0.0002	0.005	0.0010
n-Hexane	0.0009	0.021	0.0039
Cyclohexane	0.0003	0.008	0.0014
Other Hexanes	0.0030	0.073	0.0133
Heptanes	0.0013	0.031	0.0056
Methylcyclohexane	0.0004	0.009	0.0016
2,2,4-Trimethylpentane	0.0001	0.003	0.0005
Benzene	0.0002	0.006	0.0010
Toluene	0.0003	0.006	0.0011
Ethylbenzene	0.0002	0.005	0.0010
Xylenes	0.0002	0.005	0.0008
C8+ Heavies	<0.0001	0.001	0.0001
Total Emissions	0.4536	10.886	1.9867
Total Hydrocarbon Emissions	0.4536	10.886	1.9867
Total VOC Emissions	0.0574	1.378	0.2514
Total HAP Emissions	0.0019	0.046	0.0084
Total BTEX Emissions	0.0009	0.022	0.0040

FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Methane Ethane Propane Isobutane n-Butane	10.8052 9.0042 1.5443 0.3063 0.4366	259.325 216.101 37.062 7.350 10.478	47.3269 39.4384 6.7639 1.3414 1.9122
Isopentane	0.1426	3.422	0.6245

			Page: 3
n-Pentane	0.0834	2.001	0.3651
Cyclopentane	0.0109	0.262	0.0478
n-Hexane	0.0441	1.058	0.1930
Cyclohexane	0.0157	0.376	0.0686
Other Hexanes	0.1520	3.647	0.6656
Heptanes	0.0636	1.527	0.2787
Methylcyclohexane	0.0179	0.430	0.0784
2,2,4-Trimethylpentane	0.0060	0.143	0.0262
Benzene	0.0118	0.282	0.0515
Toluene	0.0130	0.312	0.0570
Ethylbenzene	0.0111	0.267	0.0488
Xylenes	0.0095	0.227	0.0415
C8+ Heavies	0.0016	0.039	0.0071
Total Emissions	22.6796	544.310	99.3366
Total Hydrocarbon Emissions	22 (70)	E44 310	00 2266
Total VOC Emissions	22.6796	544.310	99.3366
	2.8702	68.884	12.5713
Total HAP Emissions	0.0954	2.290	0.4180
Total BTEX Emissions	0.0454	1.089	0.1988

EQUIPMENT REPORTS:

COMBUSTION DEVICE -----

Ambient Temperature: 60.00 deg. F
Excess Oxygen: 2.00 %
Combustion Efficiency: 98.00 %
Supplemental Fuel Requirement: 1.15e-001 MM BTU/hr

Component	Emitted	Destroyed
Methane Ethane Propane Isobutane n-Butane	2.00% 2.00% 2.00% 2.00% 2.00%	98.00%
Isopentane	2.00%	98.00%
n-Pentane	2.00%	98.00%
Cyclopentane	2.00%	98.00%
n-Hexane	2.00%	98.00%
Cyclohexane	2.00%	98.00%
Other Hexanes	2.00%	98.00%
Heptanes	2.00%	98.00%
Methylcyclohexane	2.00%	98.00%
2,2,4-Trimethylpentane	2.00%	98.00%
Benzene	2.00%	98.00%
Toluene	2.00%	98.00%
Ethylbenzene	2.00%	98.00%
Xylenes	2.00%	98.00%
C8+ Heavies	2.00%	98.00%

ABSORBER

NOTE: Because the Calculated Absorber Stages was below the minimum allowed, GRI-GLYCalc has set the number of Absorber Stages to 1.25 and has calculated a revised Dry Gas Dew Point.

Calculated Absorber Stages: 1.25 clculated Dry Gas Dew Point: 0.30 lbs. H2O/MMSCF Calculated Dry Gas Dew Point:

Temperature: 45.0 deg. F
Pressure: 650.0 psig
Dry Gas Flow Rate: 60.0000 MMSCF/day
Glycol Losses with Dry Gas: 0.0302 lb/hr

Wet Gas Water Content: Saturated

Calculated Wet Gas Water Content: 13.40 lbs. H2O/MMSCF Calculated Lean Glycol Recirc. Ratio: 18.31 gal/lb H2O

Component	Remaining in Dry Gas	Absorbed in Glycol
Water Carbon Dioxide Nitrogen Methane Ethane	2.21% 99.73% 99.99% 99.99%	97.79% 0.27% 0.01% 0.01% 0.05%
Propane	99.90%	0.10%
Isobutane	99.84%	0.16%
n-Butane	99.78%	0.22%
Isopentane	99.76%	0.24%
n-Pentane	99.67%	0.33%
Cyclopentane	98.49%	1.51%
n-Hexane	99.35%	0.65%
Cyclohexane	96.93%	3.07%
Other Hexanes	99.53%	0.47%
Heptanes	98.59%	1.41%
Methylcyclohexane	96.23%	3.77%
2,2,4-Trimethylpentane	99.45%	0.55%
Benzene	70.63%	29.37%
Toluene	57.03%	42.97%
Ethylbenzene	44.61%	55.39%
Xylenes	33.84%	66.16%
C8+ Heavies	98.49%	1.51%

FLASH TANK

Flash Control: Combustion device

Flash Control Efficiency: 98.00 %
Flash Temperature: 135.0 deg. F
Flash Pressure: 35.0 psig

Component	Left in Glycol	Removed in Flash Gas
Water	99.96%	0.04%
Carbon Dioxide	41.31%	58.69%
Nitrogen	5.89%	94.11%
Methane	5.95%	94.05%
Ethane	18.59%	81.41%
Propane	31.29%	68.71%
Isobutane	40.86%	59.14%
n-Butane	47.34%	52.66%
Isopentane	51.08%	48.92%
n-Pentane	56.53%	43.47%

		Page:	5
Cyclopentane	84.43%	15.57%	
n-Hexane	70.22%	29.78%	
Cyclohexane	91.08%	8.92%	
Other Hexanes	64.44%	35.56%	
Heptanes	83.05%	16.95%	
Methylcyclohexane	92.95%	7.05%	
2,2,4-Trimethylpentane	71.66%	28.34%	
Benzene	98.52%	1.48%	
Toluene	99.08%	0.92%	
E thylbenzene	99.48%	0.52%	
VIII on o a	00 648	0.368	
Xylenes	99.64%	0.36%	
C8+ Heavies	98.33%	1.67%	

REGENERATOR

Regenerator Stripping Gas:

Dry Product Gas

Stripping Gas Flow Rate: 4.4000 scfm

Component	Remaining in Glycol	Distilled Overhead
Water	63.25%	36.75%
Carbon Dioxide	0.00%	100.00%
Nitrogen	0.00%	100.00%
Methane	0.00%	100.00%
Ethane	0.00%	100.00%
Propane	0.00%	100.00%
Isobutane	0.00%	100.00%
n-Butane	0.00%	100.00%
Isopentane	0.98%	99.02%
n-Pentane	0.88%	99.12%
Cyclopentane	0.59%	99.41%
n-Hexane	0.71%	99.29%
Cyclohexane	3.51%	96.49%
Other Hexanes	1.55%	98.45%
Heptanes	0.60%	99.40%
Methylcyclohexane	4.30%	95.70%
2,2,4-Trimethylpentane	2.09%	97.91%
Benzene	5.08%	94.92%
Toluene	7.97%	92.03%
Ethylbenzene	10.46%	89.54%
Xylenes	12.95%	87.05%
C8+ Heavies	12.24%	87.76%

STREAM REPORTS:

WET GAS STREAM

Temperature: 45.00 deg. F Pressure: 664.70 psia Flow Rate: 2.50e+006 scfh

Component

Conc. Loading (vol%) (lb/hr)

```
Water 2.82e-002 3.35e+001
              Carbon Dioxide 1.49e-001 4.32e+002
                    Nitrogen 3.87e-001 7.14e+002
                     Methane 8.72e+001 9.22e+004
                      Ethane 1.12e+001 2.21e+004
                     Propane 8.08e-001 2.35e+003
                   Isobutane 8.70e-002 3.33e+002
                   n-Butane 9.90e-002 3.79e+002
                  Isopentane 2.50e-002 1.19e+002
                   n-Pentane 1.20e-002 5.71e+001
                Cyclopentane 1.00e-003 4.62e+000
                    n-Hexane 4.00e-003 2.27e+001
                 Cyclohexane 1.00e-003 5.55e+000
               Other Hexanes 1.60e-002 9.09e+001
                    Heptanes 4.00e-003 2.64e+001
           Methylcyclohexane 1.00e-003 6.47e+000
       2,2,4-Trimethylpentane 5.00e-004 3.76e+000
                     Benzene 5.00e-004 2.57e+000
                     Toluene 5.00e-004 3.04e+000
                Ethylbenzene 5.00e-004 3.50e+000
                     Xylenes 5.00e-004 3.50e+000
                C8+ Heavies 5.00e-004 5.61e+000
            Total Components 100.00 1.19e+005
```

DRY GAS STREAM

Temperature: 45.00 deg. F

Temperature: 45.00 deg. F Pressure: 664.70 psia Flow Rate: 2.50e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	6.25e-004 1.49e-001 3.87e-001 8.72e+001 1.12e+001	4.31e+002 7.14e+002
Isobu [†] tane n-Butane Isopentane	8.07e-001 8.69e-002 9.88e-002 2.49e-002 1.20e-002	3.33e+002 3.78e+002 1.19e+002
Cyclohexane Other Hexanes	3.97e-003 9.69e-004	2.26e+001 5.38e+000 9.04e+001
	4.97e-004 3.53e-004 2.85e-004	3.74e+000 1.82e+000 1.73e+000
Xylenes C8+ Heavies Total Components		

LEAN GLYCOL STREAM

Temperature: 45.00 deg. F Flow Rate: 1.00e+001 gpm

Component Conc. Loading (wt%) (lb/hr) TEG 9.90e+001 5.58e+003 Water 1.00e+000 5.63e+001 Carbon Dioxide 2.05e-012 1.15e-010 Nitrogen 1.79e-013 1.01e-011 Methane 6.85e-018 3.86e-016 Ethane 9.27e-008 5.22e-006 Propane 1.62e-009 9.15e-008 Isobutane 2.76e-010 1.55e-008 n-Butane 3.65e-010 2.06e-008 Isopentane 2.59e-005 1.46e-003 n-Pentane 1.70e-005 9.59e-004 Cyclopentane 6.22e-006 3.51e-004 n-Hexane 1.31e-005 7.40e-004 Cyclohexane 9.98e-005 5.62e-003 Other Hexanes 7.59e-005 4.27e-003 Heptanes 3.33e-005 1.88e-003 Methylcyclohexane 1.80e-004 1.02e-002 2,2,4-Trimethylpentane 5.61e-006 3.16e-004 Benzene 7.06e-004 3.98e-002 Toluene 1.99e-003 1.12e-001 Ethylbenzene 3.99e-003 2.25e-001 Xylenes 6.09e-003 3.43e-001 C8+ Heavies 2.06e-004 1.16e-002 --------Total Components 100.00 5.63e+003

RICH GLYCOL STREAM

Temperature: 45.00 deg. F Pressure: 664.70 psia Flow Rate: 1.01e+001 gpm

NOTE: Stream has more than one phase.

Component	Conc. (wt%)	Loading (lb/hr)
Water Carbon Dioxide Nitrogen	9.78e+001 1.56e+000 2.02e-002 1.77e-003 2.02e-001	8.91e+001 1.15e+000 1.01e-001
Propane Isobutane	1.94e-001 3.94e-002 9.08e-003 1.45e-002 5.11e-003	2.25e+000 5.18e-001 8.29e-001
Cyclopentane	2.60e-003 3.08e-003	7.01e-002 1.48e-001 1.76e-001

```
Heptanes 6.58e-003 3.75e-001
Methylcyclohexane 4.46e-003 2.54e-001
2,2,4-Trimethylpentane 3.70e-004 2.11e-002
Benzene 1.40e-002 7.96e-001
Toluene 2.48e-002 1.42e+000

Ethylbenzene 3.79e-002 2.16e+000
Xylenes 4.66e-002 2.66e+000
C8+ Heavies 1.69e-003 9.65e-002

Total Components 100.00 5.70e+003
```

FLASH TANK OFF GAS STREAM

Temperature: 135.00 deg. F Pressure: 49.70 psia Flow Rate: 3.98e+002 scfh

Component Conc. Loading (vol%) (lb/hr) Water 1.89e-001 3.57e-002 Carbon Dioxide 1.47e+000 6.77e-001 Nitrogen 3.23e-001 9.48e-002 Methane 6.42e+001 1.08e+001 Ethane 2.86e+001 9.00e+000 Propane 3.34e+000 1.54e+000 Isobutane 5.02e-001 3.06e-001 n-Butane 7.16e-001 4.37e-001 Isopentane 1.88e-001 1.43e-001 n-Pentane 1.10e-001 8.34e-002 Cyclopentane 1.48e-002 1.09e-002 n-Hexane 4.88e-002 4.41e-002 Cyclohexane 1.78e-002 1.57e-002 Other Hexanes 1.68e-001 1.52e-001 Heptanes 6.05e-002 6.36e-002 Methylcyclohexane 1.74e-002 1.79e-002 2,2,4-Trimethylpentane 4.99e-003 5.98e-003 Benzene 1.43e-002 1.18e-002 Toluene 1.35e-002 1.30e-002 Ethylbenzene 1.00e-002 1.11e-002 Xylenes 8.51e-003 9.47e-003 C8+ Heavies 9.03e-004 1.61e-003 -----Total Components 100.00 2.35e+001

FLASH TANK GLYCOL STREAM

Temperature: 135.00 deg. F Flow Rate: 1.01e+001 gpm

Component Conc. Loading (wt%) (lb/hr)

TEG 9.82e+001 5.58e+003
Water 1.57e+000 8.91e+001
Carbon Dioxide 8.39e-003 4.77e-001
Nitrogen 1.04e-004 5.93e-003
Methane 1.20e-002 6.83e-001

Ethane 3.62e-002 2.06e+000
Propane 1.24e-002 7.03e-001

```
Isobutane 3.73e-003 2.12e-001
             n-Butane 6.91e-003 3.92e-001
           Isopentane 2.62e-003 1.49e-001
            n-Pentane 1.91e-003 1.08e-001
         Cyclopentane 1.04e-003 5.92e-002
            n-Hexane 1.83e-003 1.04e-001
          Cyclohexane 2.82e-003 1.60e-001
        Other Hexanes 4.85e-003 2.75e-001
             Heptanes 5.49e-003 3.12e-001
    Methylcyclohexane 4.16e-003 2.36e-001
2,2,4-Trimethylpentane 2.66e-004 1.51e-002
              Benzene 1.38e-002 7.84e-001
              Toluene 2.47e-002 1.40e+000
         Ethylbenzene 3.79e-002 2.15e+000
             Xylenes 4.66e-002 2.65e+000
         C8+ Heavies 1.67e-003 9.49e-002
       Total Components 100.00 5.68e+003
```

FLASH GAS EMISSIONS

Flow Rate: 1.49e+003 scfh

Control Method: Combustion Device

Control Efficiency: 98.00

Component Conc. Loading (vol%) (lb/hr) Water 6.23e+001 4.41e+001 Carbon Dioxide 3.71e+001 6.41e+001 Nitrogen 8.62e-002 9.48e-002 Methane 3.43e-001 2.16e-001 Ethane 1.53e-001 1.80e-001 Propane 1.78e-002 3.09e-002 Isobutane 2.68e-003 6.13e-003 n-Butane 3.83e-003 8.73e-003 Isopentane 1.01e-003 2.85e-003 n-Pentane 5.88e-004 1.67e-003 Cyclopentane 7.93e-005 2.18e-004 n-Hexane 2.60e-004 8.81e-004 Cyclohexane 9.48e-005 3.13e-004 Other Hexanes 8.98e-004 3.04e-003 Heptanes 3.23e-004 1.27e-003 Methylcyclohexane 9.29e-005 3.58e-004 2,2,4-Trimethylpentane 2.66e-005 1.20e-004 Benzene 7.66e-005 2.35e-004 Toluene 7.19e-005 2.60e-004 Ethylbenzene 5.35e-005 2.23e-004 Xylenes 4.54e-005 1.89e-004 C8+ Heavies 4.83e-006 3.23e-005

REGENERATOR OVERHEADS STREAM

Total Components 100.00 1.09e+002

Temperature: 212.00 deg. F Pressure: 14.70 psia Flow Rate: 1.04e+003 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	6.63e+001 4.33e-001 1.06e-001 2.37e+001 5.33e+000	5.22e-001 8.14e-002 1.04e+001
Isobutane n-Butane Isopentane	7.87e-001 1.55e-001 2.71e-001 8.08e-002 5.73e-002	2.47e-001 4.32e-001 1.60e-001
Cyclohexane Other Hexanes	4.47e-002 6.72e-002	1.06e-001 1.55e-001 2.81e-001
Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene	4.85e-003 3.48e-001 5.11e-001	1.52e-002 7.44e-001 1.29e+000
Xylenes C8+ Heavies Total Components		

COMBUSTION DEVICE OFF GAS STREAM

Temperature: 1000.00 deg. F Pressure: 14.70 psia Flow Rate: 6.90e+000 scfh

Component	Conc. (vol%)	
Ethane Propane Isobutane	7.14e+001 1.61e+001 2.37e+000 4.67e-001 8.18e-001	8.78e-002 1.90e-002 4.93e-003
Cyclopentane	1.73e-001 9.30e-002 1.35e-001	2.27e-003 1.19e-003 2.11e-003
Methylcycloĥexane 2,2,4-Trimethylpentane	3.43e-001 2.54e-001	6.25e-003 4.53e-003 3.04e-004
Ethylbenzene	2.39e+000 5.42e-002	3.85e-002 4.61e-002 1.68e-003



Certificate of Analysis Number: 2030-14100121-005A

Carencro Laboratory 4790 NE Evangeline Thruway Carencro, LA 70520

Gary Vermillion Gas Analytical Services PO Box 1028 Bridgeport, WV 26330

Oct. 16, 2014

Field:

EQT

Station Name: Curtisville Compressor

Sample Point: Cylinder No: 0377

Analyzed:

10/15/2014 09:14:28 by CC43

Sampled By: Sample Of:

GC-GAS

Spot Gas

Sample Date: 09/30/2014 09:45 Sample Conditions: 772 psig, @ 58 °F Method: GPA 2286

Analytical Data

			. unding	tiour Butu		
Components	Mol. %	Wt. %	GPM at 14.73 psia			
Nitrogen	0.387	0.601		GPM TOTAL C2+	3.299	
Carbon Dioxide	0.149	0.363		GPM TOTAL C3+	0.305	
Methane	87.236	77.558		GPM TOTAL iC5+	0.022	
Ethane	11.170	18.614	2.994			
Propane	0.808	1.975	0.224			
Iso-Butane	0.087	0.280	0.028			
n-Butane	0.099	0.319	0.031			
Iso-Pentane	0.025	0.100	0.009			
n-Pentane	0.012	0.048	0.004			
Hexanes	0.021	0.074	0.006			
Heptanes Plus	0.006	0.068	0.003			
	100.000	100.000	3.299			
Physical Properties			Total	C7+		
Relative Density Rea	l Gas		0.6244	3.6850		
Calculated Molecular	· Weight		18.04	106.73		
Compressibility Factor	or Č		0.9974			
GPA 2172-09 Calcul						
Calculated Gross B	TU per ft ^a @	14.73 psia	& 60°F			
Real Gas Dry BTU			1114	5751		
Water Sat. Gas Base	BTU		1094	5651		
Comments: H2O M	lol% : 1.740	; Wt% : 1.73	38			

Hydrocarbon Laboratory Manager

Quality Assurance:

The above analyses are performed in accordance with ASTM, UOP, GPA guidelines for quality assurance, unless otherwise stated.



Certificate of Analysis

Number: 2030-14100121-005A

Carencro Laboratory 4790 NE Evangeline Thruway Carencro, LA 70520

Gary Vermillion Gas Analytical Services PO Box 1028 Bridgeport, WV 26330

EQT Field:

Station Name: Curtisville Compressor

Sample Point:

Cylinder No: 0377

Analyzed:

10/15/2014 09:14:28 by CC43

GC-GAS

Sampled By: Sample Of:

Spot Gas

Oct. 16, 2014

Sample Date: 09/30/2014 09:45 Sample Conditions:772 psig, @ 58 °F Method: GPA 2286

Analytical Data

Components	Mol. %	Wt. %	
Carbon Dioxide	0.149	0.363	
Hydrogen Sulfide	N/R	N/R	
Nitrogen	0.387	0.601	
Methane	87.236	77.558	
Ethane	11,170	18.614	
Propane	0.808	1.975	
Iso-Butane	0.087	0.280	
n-Butane	0.099	0.319	
Iso-Pentane	0.025	0.100	
n-Pentane	0.012	0.048	
Cyclopentane	0.001	0.003	
n-Hexane	0.004	0.016	
Cyclohexane	0.001	0.003	
Other Hexanes	0.016	0.050	
n-Heptane	0.001	0.006	
Other Heptanes	0.003	0.028	
Methylcyclohexane	0.001	0.005	
2,2,4-Trimethylpentane	NIL	NIL	
Benzene	NIL	0.002	
Toluene	NIL	0.002	
Ethylbenzene	NIL	NIL	
Xylenes	NIL	0.002	
C8 + Heavies	NIL	0.025	
	100.000	100.000	
	. 50.000		

Hydrocarbon Laboratory Manager

Fatti L. Perro

ATTACHMENT O

Monitoring/Recordkeeping/Reporting/Testing Plans

Monitoring, Recording, Reporting, and Testing Plan

Plan Type	Emission Unit	Pollutant	Requirements	Frequency	Method of Measurement
Monitoring	Glycol Dehydration Units	N/A	Natural Gas Throughput	Annual	Flow Meter
Record Keeping	Glycol Dehydration Units	VOC/HAP	Maintain emissions below permit limits.	Annual	GRI_GLY Calc

ATTACHMENT P

Public Notice

AIR QUALITY PERMIT NOTICE Notice of Application

Notice is given that Equitrans, LP has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a construction permit application for an existing natural gas compressor station (the Curtisville Compressor Station) located off Laurel Run Road near Mannington in Marion County, West Virginia. The site latitude and longitude coordinates are: 39.52345 N, -80.43980 W. The proposed change includes the replacement of the existing dehydration unit with a new unit, which will be completed in 2019.

The applicant estimates the potential increase in the following Regulated Air Pollutants associated with the project will be:

Particulate Matter (PM) = 0.23 tpy
Sulfur Dioxide (SO2) = 0.02 tpy
Volatile Organic Compounds (VOC) = 1.45 tpy
Carbon Monoxide (CO) = 2.49 tpy
Nitrogen Oxides (NOx) = 2.96 tpy
Total Hazardous Air Pollutants (HAPs) = 0.69 tpy
n-hexane = 0.03 tpy
Toluene = 0.14 tpy
Ethylbenzene = 0.20 tpy
Benzene = 0.08 tpy
Xylenes = 0.24 tpy
Carbon Dioxide Equivalents (CO₂e) = 3,905 tpy

Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1250, during normal business hours.

Dated on [INSERT DATE]

By: Equitrans, LP

Jack Mackin, Vice President of Operations

2200 Energy Dr.

Canonsburg, PA 15317

ATTACHMENT S

Title V Permit Revision Information

Attachment S

Title V Permit Revision Information

1. New Applicable Requirements Summary				
Mark all applicable requirements associated with the change	es involved with this permit revision:			
⊠ SIP	☐ FIP			
Minor source NSR (45CSR13)	☐ PSD (45CSR14)			
☐ NESHAP (45CSR15)	☐ Nonattainment NSR (45CSR19)			
Section 111 NSPS (Subpart(s))	Section 112(d) MACT standards (Subpart(s))			
Section 112(g) Case-by-case MACT	☐ 112(r) RMP			
Section 112(i) Early reduction of HAP	Consumer/commercial prod. reqts., section 183(e)			
Section 129 Standards/Reqts.	Stratospheric ozone (Title VI)			
Tank vessel reqt., section 183(f)	☐ Emissions cap 45CSR§30-2.6.1			
NAAQS, increments or visibility (temp. sources)	45CSR27 State enforceable only rule			
45CSR4 State enforceable only rule	☐ Acid Rain (Title IV, 45CSR33)			
☐ Emissions Trading and Banking (45CSR28)	Compliance Assurance Monitoring (40CFR64) (1)			
□ NO _x Budget Trading Program Non-EGUs (45CSR1)	□ NO _x Budget Trading Program EGUs (45CSR26)			
(1) If this box is checked, please include Compliance Assuspecific Emission Unit (PSEU) (See Attachment H to Title explain why Compliance Assurance Monitoring is not ap There are no large pollutant specific emission units.	V Application). If this box is not checked, please plicable:			
I nere are no large pollutant specific emission units.	Therefore, CAW is not required at this time.			
2. Non Applicability Determinations				
List all requirements, which the source has determined permit shield is requested. The listing shall also include	not applicable to this permit revision and for which a e the rule citation and a rationale for the determination.			
Permit Shield Requested (not applicable to Minor Modifications)				

All of the required forms and additional info	rmation can be found i	under the Pe	rmitting Section of DAQ's website, or requested by phone.	
3. Suggested Title V Draft Permit L	anguage			
revision? Yes No If Yes Also, please provide Suggested (including all applicable requiren /recordkeeping/ reporting requires	es, describe the char Fitle V Draft Perionents associated with ments), OR attach mit or Consent Ore	nges belov mit langua vith the pe a marked der numbe	sion outside of the scope of the NSR Permit v. age for the proposed Title V Permit revision rmit revision and any associated monitoring up pages of current Title V Permit. Please or, condition number and/or rule citation (e.g.	
4. Active NSR Permits/Permit Deter	rminations/Conse	nt Orders	Associated With This Permit Revision	
Permit or Consent Order Number	Date of Issu	ance	Permit/Consent Order Condition Number	
NA				
	1 1			
5. Inactive NSR Permits/Obsolete P	ermit or Consent	Orders Co	onditions Associated With This Revision	
Permit or Consent Order Number	Date of Issua	nnce	Permit/Consent Order Condition Number	
NA				
	1 1			
6. Change in Potential Emissions		r -		
Pollutant		Change in Potential Emissions (+ or -), TPY		
PM			0.23	
SO2			0.02	
СО			2.49	
NOx			2.96	

Pollutant	Change in Potential Emissions (+ or -), TPY
PM	0.23
SO2	0.02
СО	2.49
NOx	2.96
НАР	0.69
VOC	1.45
N-Hexane	0.03
Benzene	0.08
CO2(e)	3,905

		on For Use Of Minor Modification	n Procedures (Require	d Only for Minor Modification
Note	certi	certification must be signed by fication will be returned as inc ification Procedures are as follows	omplete. The criteria	Applications without a sign for allowing the use of Min
	i. Provide ii. Provide iii. Pro	oposed changes do not violate any oposed changes do not involve stordkeeping requirements in the perposed changes do not require chitation or other standard, or a bient air quality impacts, or a visit oposed changes do not seek to estand underlying applicable requirement applicable requirement to which the chitems and conditions include, be at the avoid classification as a modification in the chitems and conditions include, be at the avoid classification as a modification in the conditions include and the conditions include the chitems and 45CSR19; oposed changes do not involve precedent in the condition of the condition in the	applicable requirement; significant changes to emit; or change a case-by-ca source-specific determibility increment analysis; blish or change a permit ent and which permit of the source would other ut are not limited to a felification under any proporegulations promulgate econstruction review under any rule of the	ination for temporary sources in term or condition for which the condition has been used to average be subject (synthetic minor ederally enforceable emissions of vision of Title I or any alternatived under § 112(j)(5) of the Clear Title I of the Clean Air Act be Director to be processed as
proc perr proc the	cedures may mits, emissior cedures are ex State Impleme	subparagraph 45CSR§30-6.5.a.1.4 be used for permit modifications is trading, and other similar approplicitly provided for in rules of the entation Plan under the Clean Air Aissued under 45CSR30.	s involving the use of paches, to the extent that Director which are app	economic incentives, marketal at such minor permit modification roved by the U.S. EPA as a part
of N	Minor permit	SR§30-6.5.a.2.C., the proposed r modification procedures as set 1 tion procedures are hereby reque	orth in Section 45CSR	§30-6.5.a.1.A. The use of Min
of N	Minor permit mit modificat	modification procedures as set f	orth in Section 45CSR	§30-6.5.a.1.A. The use of Min
of M peri	Minor permit mit modificat	modification procedures as set f	orth in Section 45CSR ested for processing of	§30-6.5.a.1.A. The use of Min
of M peri	dinor permit mit modificate i): (typed): Compliance	modification procedures as set fition procedures are hereby reque	Orth in Section 45CSR ested for processing of the Date: Title:	§30-6.5.a.1.A. The use of Minthis application. (Please use blue ink)
of M peri	Minor permit mit modificate (typed): Compliance Suggested T	modification procedures as set ition procedures are hereby requestion procedures as set it in the procedures are hereby requestion p	Date: Title:	§30-6.5.a.1.A. The use of Minthis application.